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S/120/62/000/004/010/047  
EO32/E514

24.6730

AUTHORS: Vladimirskiy, V.V., Kobozay, A.S., Marfenko, S.V.,  
Pevnev, A.K., Porubny, N.I. and Tarasov, Ye.K.TITLE: Effect of the deformation of the foundations on the  
orbit of protons in a synchrotron

PERIODICAL: Pribory i tekhnika eksperimenta, no.4, 1962, 66-69

TEXT: Unavoidable displacements of the ground in the vertical and horizontal directions due to seasonal variations in the temperature, humidity and so on, may give rise to relative displacements in the position of magnet sections, which in turn may produce forced oscillations of the proton beam. In the 7 GeV proton synchrotron of the GKAE the magnet is supported by a continuous solid ring which is in principle similar to that employed at CERN. The reinforced-concrete ring which supports the magnet lies directly on the ground which consists of soft morainic deposits. The relatively small dimensions of the ring ( $R = 40$  m) ensured that it could be made sufficiently rigid and thereby minimise the effect of nonuniform settling of the ground on the orbit. The ring was placed at a depth of 5 m. A theoretical

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Effect of the deformation of the ... S/120/62/000/004/010/047  
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analysis is now given of the strength of the ring foundation by developing the displacement of the axis of the accelerator chamber due to deformation of the foundations into a Fourier series. Owing to the rigidity of the magnet sections and the small distance between neighbouring sections, the position of all the sections can be specified with sufficient accuracy by the coordinates of 112 points. The Fourier series, therefore, contain a finite number of terms. For each harmonic of the deformation one can then calculate the amplitude of the corresponding periodic orbits. Numerical calculations showed that the 13th, 43rd and neighbouring harmonics were the most dangerous. The mathematical analysis is facilitated by the fact that a mathematical solution is available for the problem of mechanical vibrations of an elastic ring (Love, Mathematical Theory of Elasticity). In their final form the foundations were in the shape of a continuous reinforced-concrete belt of square cross-section having a length of 250 m, height 5 m and width 5 m with a nett load of about 16 tons per running metre. The belt contains two circular cable tunnels ( $1.25 \times 1.95 \text{ m}^2$ ). The analytical

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calculations and the design data were then tested experimentally by observations of the position of 28 markers attached to the foundations. Vertical and radial variations for the period 1959/62 are reported in the form of graphs, from which it is concluded that the maximum departure of the orbit from the axis of the chamber, due to the deformation of the foundations, did not exceed 1.5 mm. The amplitude of the deformations of the foundations was of the same order of magnitude (about 1 mm). There are 2 figures and 2 tables.

ASSOCIATION: Institut teoreticheskoy i eksperimental'noy fiziki GKAE  
(Institute of Theoretical and Experimental Physics  
GKAE)

SUBMITTED: March 31, 1962

Card 3/3

KOBOZEV, G. V., Cand Med Sci -- (diss) "Apparatus for frontal micro-electrophoresis with optical registration and its application to the study of adsorption properties of proteins in blood serum." Simferopol', 1960. 20 pp; (Krymskiy State Medical Inst im I. V. Stalin); 200 copies; price not given; (KL, 17-60, 169)

TROITSKIY, G.V.; KOBOZEV, G.V.

Design of precision spectropolarimeters used for protein  
studies. Biokhimiia 28 no.6:992-998 N-D'63 (MIRA 17:1)

1. Chair of Biological Chemistry, Medical Institute, Simferopol'.

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DATE 07-17-2014 BY SP000723410014-9

USSR/Medicine - Pathophysiology

FD-2561

Card 1/1      Pub. 17-14/23

Author        : Meyerson, F. Z.; Kobozev, G. V.

Title         : On a method for forming an experimental stenosis of the aorta

Periodical    : Byul. eksp. biol. i med. 5, 50-52, May 1955

Abstract      : Describes a method for forming an experimental stenosis of the aorta in rabbits which permits the following: constriction of the aorta following an appreciable interval of time after the operation, gradual constriction of the aorta, and removal of the ligature after a period of constriction of the aorta without requiring a second operation. Diagrams. Three references, two of them USSR (since 1940).

Institution    : Central Scientific Research Institute of Physical Methods for Therapy imeni I. M. Sechenov (Director O. V. Glebova), Yalta

Submitted     : July 22, 1954 by Academician A. D. Speranskiy

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DATE 07-17-2014 BY SP000723410014-9

APPROVED FOR RELEASE: 09/18/2001 CIA-RDP86-00513R000723410014-9

Integral graded salivograph. Zh. vys. nerv. deiat. 5 no.6:912-915  
N-D '55. (MLRA 9:3)

1. Institut fizicheskikh metodov lecheniya imeni. I.M. Sechenova,  
Yalta.

(SALIVATION.  
registration with integral graded salivograph)

MEYERSON, F.Z.; KOBZHEV, O.V.

Method of producing experimental stenosis of the aorta. Biul.eksp.  
biol.i med. 39 no.5:50-52 My '55. (MLRA 8:7)

1. Iz Tsentral'nogo nauchno-issledovatel'skogo institut fizicheskikh  
metodov lecheniya imeni I.M.Sechanova (dir. O.V.Glebova), Yalta.  
Predstavlena akademikom A.D.Speranskim.  
(AORTIC, VALVE, stenosis,  
exper., technic of prod.)

А. Г. ТРОИЦКИЙ  
КОБОЗЕВ, О. В.

Use of mechanical coulometer in protein electrophoresis [with summary in English]. Ukr.biokhim. zhur. 29 no.3:375-392 '57.  
(MIRA 10:9)

1. Kafedra biokhimii Krymskogo meditsinskogo instituta,  
g. Sineropol'.  
(VOLTMETER) (ELECTROPHORESIS)  
(PROTEINS-ANALYSIS)

ТРОИЦКИЙ, О. В., КОБОЗЕВ, О. В.  
APPROVED FOR RELEASE: 09/18/2001

CIA-RDP86-00513R000723410014-9

Further improvement of the apparatus for protein electrophoresis [with summary in English]. Biokhimiia 23 no.6:869-878 E-D '58  
(MIRA 11:12)

1. Kafedra biologicheskoy khimii Krymskogo meditsinskogo instituta  
Sineropol'.  
(ELECTROPHORESIS)

KOBOKINA, O.M.; KOBOKIN, O.V.

Method of using small quantities of serum for paper electrophoresis, Lab. de lo 6 no, 3157-58 Ny-Te 160.  
(PAPER ELECTROPHORESIS) (SERUM) (NIMA 13:7)

KOBOZEV, G. V., (USSR)

"A Cuvette for Frontal Electrophoresis, made  
of Organic Glass with Cooling."

Report presented at the 5th Int'l. Biochemistry Congress,  
Moscow, 10-16 Aug 1961.

KOBZEV, I. I., MINER-HYDROGEOLOGIST

MIN/Geophysics - Hot-Spring Minerals

Mar 52

"New Sources of Minerals," I. I. Kobzey, Engr.-Hydrogeologist

"Priroda" Vol. 41, No. 3, pp 119, 120

States that underground waters, by circulating through mineral deposits in the depths of the earth, are often enriched with salts and gases and thus can form mineral sources where they exit at the surface; e.g., at the hot springs of Staraya Russa, Sol'tsy, Kamchatka, northern

230758

Urals, etc. States that a theoretical study must be made to det the conditions of temp and solv. that govern possible sources of minerals. Mentions work on Sakhalin to exploit the mud pots there, and also so-called "sifoids," as sources of CO<sub>2</sub>.

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CIA-RDP86-00513R000723410014-9

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CIA-RDP86-00513R000723410014-9"

KOBOTIN, I.

New occurrence of carbonic acid saline-alkaline waters like those of  
springs nos. 17 and 4 in Yessentuki. Vop.kur.fizioter. i lech. fiz.  
kal't. 21 no.3:95-96 Jl-8 '56. (MLRA 9:10)  
(NOVOSIBIRSK--MINERAL WATERS)

Card 1/1

0<sup>o</sup>

Oxidation of nitric oxide to nitrogen pentoxide by means of ozone in the direct electric discharge. N. I. Makarova, M. Tsvetko and S. Prokof'yev. J. Russ. Chem. (U. R. S. S.) 3, No. 4 (1932). With a horizontal condenser connected to a 10,000-v. transformer, a study was made of the reaction:  $2NO + 3O_3 \rightarrow N_2O_5 + 3O_2$ . A rate of 0.33  $\pm$  0.02 l./min. of air through the condenser resulted in an 1% content of  $N_2O_5$  by vol. The  $NO$  was mixed with  $N_2$  in the ratio 10:91 and the mixt. passed into the measured air at a rate of 10 cc./min. In this case the  $O_3$  was in excess of the theoretical amt. required and the reaction was almost instantaneous, 95% of the  $NO$  being oxidized. The ratio between  $O_3$  and the  $HNO_3$  obtained varied between 1.231 and 1.91 and was, on the av., 1.48. Hence the rate of disappearance of  $O_3$  in the presence of  $N_2O_5$  was too slow to be effective. By using the same rates of gases, but introducing the  $NO + N_2$  mixt. before the air before it was measured,  $N_2O_5$  was found in the resulting mixt., but not  $O_3$  or  $N_2O_4$ . However, when the ratio  $NO:N_2$  was changed from 10:91 to 1:99, and the mixt. was introduced into the air before it passed through the condenser (the rates of all gases were the same as above),  $O_3$  and  $N_2O_5$  but not  $NO_2$  were found in the resulting mixt. When the ratios of  $NO$  +  $N_2$  mixt. and of air were so adjusted that the amt. of  $O_3$  was less than theoretical, and the  $NO + N_2$  mixt. was introduced into the air after it passed through the condenser,  $NO_2$  alone or together with  $N_2O_5$ , depending on the amt.  $O_3$  in the air, was found.  $O_3$  had no effect on  $N_2O_5$ .

S. L. Makarova

## 610-110 METALLURGICAL LITERATURE CLASSIFICATION

C1  
A  
• Experimental studies of intermediate stages in catalysis. 1. Intermediate compounds in the catalytic reaction of hydrogen peroxide and sodium molybdate. M. I. Kharlamov and V. N. Shul'ev. J. Russ. Chem. (U. S. S. R.) 4, 273-84 (1932). Red  $\text{Na}_2\text{MoO}_4 \cdot n\text{H}_2\text{O}$  ( $n = 3.2-3$ ) is prepd. from an eq. soln. of  $\text{Na}_2\text{MoO}_4$  cooled to  $0^\circ$  by addition of  $\text{H}_2\text{O}_2$ . After it is added, the temp. is cooled to  $-30^\circ$ , and the red-brown crystals are filtered and washed with cold water, air-dried, and dried in cold air. On being heated to  $50-60^\circ$  the crystals decompose into  $\text{Na}_2\text{MoO}_4 + 2\text{O}_2$ . Yellow  $\text{Na}_2\text{MoO}_4 \cdot n\text{H}_2\text{O}$  is obtained by slow decomposition of thin layers of the red compnd. at room temp.  $\text{Na}_2\text{MoO}_4$  reacts with  $\text{H}_2\text{O}_2$  with  $\text{MoO}_4^{2-}$ ,  $\text{CrO}_4^{2-}$  and  $\text{WO}_4^{2-}$  ions and active O atoms, to give  $\text{Na}_2\text{MoO}_4$ . The heat of formation is 24 Cal. per O atom. The heats of neutralization for  $\text{H}_2\text{MoO}_4$ ,  $\text{H}_2\text{MoO}_4$ , and  $\text{H}_2\text{MoO}_4$  are 21.7, 18.3 and 6.8 Cal., resp. Thermal decomposition takes place according to the mechanism:  $\text{Na}_2\text{MoO}_4 + 4\text{H}_2\text{O} \rightarrow \text{Na}_2\text{MoO}_4 + 4\text{H}_2\text{O}_2$ ;  $2\text{H}_2\text{O}_2 \rightarrow 2\text{H}_2\text{O} + \text{O}_2$ . The catalytic decompos. with  $\text{Pt}$  is unusual, for both  $\text{Na}_2\text{MoO}_4$  and  $\text{Na}_2\text{MoO}_4$ . An intermediate  $\text{Na}_2\text{MoO}_4$  results from  $\text{Na}_2\text{MoO}_4 \rightarrow \text{Na}_2\text{MoO}_4 + \text{O}_2$ ;  $\text{Na}_2\text{MoO}_4 + \text{Na}_2\text{MoO}_4 \rightarrow 2\text{Na}_2\text{MoO}_4$ . The Arrhenius  $k_1$  values are  $10^{12.1}$  and  $10^{15.5}$ , resp., and  $\varphi = 17.4$  Cal. for both. P. H. Rathman

Experimental study of intermediate stages in catalysis. II. Kinetics of the thermal decomposition of Na permanganate in the solid state. N. I. Kabanov and N. N. Shul'ev. J. Russ. Chem. (U. S. S. R.) 6, 408-11 (1953).—The Arrhenius equation is obeyed very well by both  $\text{NaMnO}_4$  and  $\text{Na}_2\text{MnO}_4$  from  $165^\circ$  to  $180^\circ$ . The  $q$  values are 28.4 and 28.4 cal., and the  $A_0$  values are  $10^{19.0}$  and  $10^{19.6}$ , resp. The  $g/\log A_0$  values were 2.1 and 1.7, resp., for decompos. in the solid state and 1.3 and 1.7 in the dissolved state as compared with the theory for unived. gaseous decompos. Y. H. R.

Moderation of the promoter action of iron compounds was observed. M.-I. Katsuyama, B. V. Rostov, I. B. Kavrin and A. N. Sazanovskaya, *Acta Physicochim. U. R. S. S.*, 31, 126-137 (1955) (in Russian).—The promoting action of  $\text{Al}_2\text{O}_3$  and  $\text{MgO}$  on  $\text{PtO}$  was studied from the viewpoint of mixed crystals between the promoter and the initial Pt oxide. The formation of mixed crystals is to be held responsible to cause the promoting action. It was proposed that it was necessary for a promoter to be surface-active with regard to the initial state of the catalyst. A pronounced difference between the surface tensions of  $\text{PtO}_x$  and  $\text{PtO}_x + \text{Al}_2\text{O}_3$  and an absence of such a difference between  $\text{PtO}$  and  $\text{PtO} + \text{MgO}$  as confirmed by the catalytic activity of Pt reduced from these oxides were exactly shown. H. H. Rowley

H. H. Rowley

**450-110 OFFICIAL LITERATURE CLASSIFICATION**

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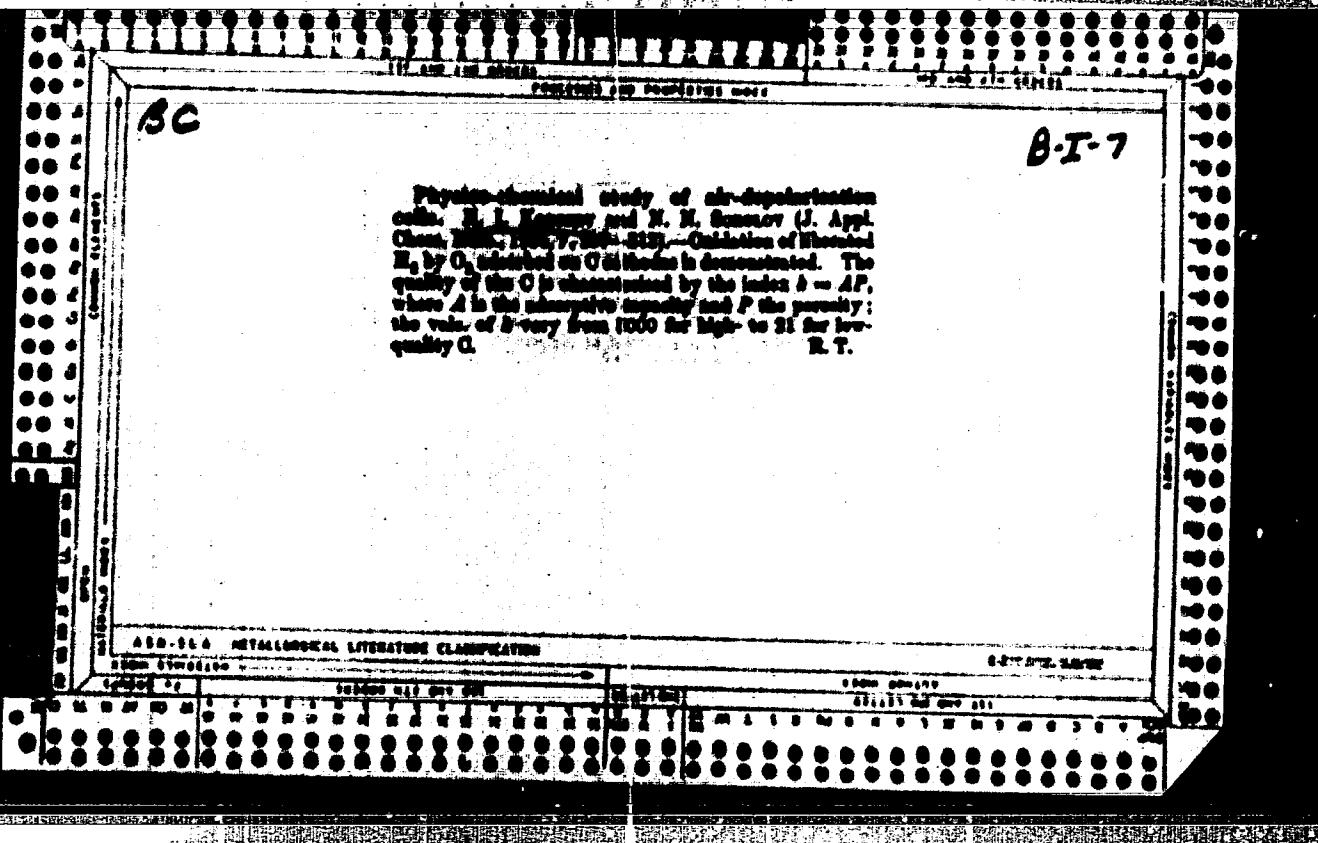
CIA-RDP86-00513R000723410014-9"

The polarization of the electromotive force of hydrogen through palladium. N. I. Kostyuk and V. Moshnikov. *Zhur. Fiz. Khim.* (USSR) 1, 811-820 (1934) (in Russian); *J. Phys. Chem. (U. S. A.)* 58, 505-524 (1934). A measurement was made of the dependence of the electromotive force of H<sub>2</sub> through a Pd membrane on the conditions of the polarizing and diffusion surfaces of the membrane. By use of H<sub>2</sub>, H<sub>2</sub>O, C<sub>2</sub>H<sub>6</sub>, glycerol and butylic acid saline, it was found that the electrodiffusion process was not influenced by the variation of phys. properties of the medium in contact with the diffusion side of the membrane. The polarization was measured by polarizing the polarization surface with pyridine, CH<sub>3</sub>(CH<sub>2</sub>)<sub>4</sub> and Na<sub>2</sub>SO<sub>4</sub>, and recorded by polarizing the diffusion surface with the same substances and H<sub>2</sub>O. The presence of electrolytes in the solution, particularly KCl and KOH, had a marked effect in regarding on the diffusion side and accelerating on the polarization side. It was shown that the diffusion took place through the intercrystalline gaps and that the edges of the crystals formed the diffusion centers. The linear dependence of the diffusion velocity on Al, the H<sub>2</sub> potential of the Pd membrane, was shown to hold for both the polarization and diffusion sides. N. N. Rostov

H. H. Lowry

**APPROVED FOR RELEASE: 09/18/2001**

CIA-RDP86-00513R000723410014-9"



*Co**4*

Catalytic influence of mercury vapor on the cracking of methane by means of glow discharge. N. I. Kofman, S. R. Vasil'ev and E. N. Gol'tsikh. Chem. Ind. (London) and U. S. S. R. 3, 280-84 (in Current 361-3) (1958).—Elect-

rodes of Al, Cu, Zn, Pb or Pt cracked CH<sub>4</sub> to yield 1.5%, C<sub>2</sub>H<sub>6</sub> and C<sub>3</sub>H<sub>8</sub>. Hg electrodes gave 8.2% uncond. hydrocarbons and heated Hg electrodes, 14%. Amalgam (2% Na) electrodes reduced the yield to less than 1%. CH<sub>4</sub> was passed through the 30-cm. tube at 30 l. per hr. at 100 mm. The electrodes were 20 mm. apart and the current was 12-18 mA. F. H. Moyer

AIAA METALLURGICAL LITERATURE CLASSIFICATION

**Inversion of the amine at equilibrium.** H. N. Ku'smin and M. I. Kostyuk. *Acta Physicochim. U. R. S. S.* 3, 191 (1937) (in German). *J. Phys. Chem.* (U. S.) 61, 71 (1937).—On the basis of heat-capacity data of Bryant (C. A. 37, 2807), E. and K. check for the amine-reaction  $\Delta F^\circ = -18,343 + 34,773 T \ln T - 0.01794 T^2 + 0.0000000 T^3 - 48,45 T$ . Up to  $1000^\circ$  this agrees well with the equation used by Masted (C. A. 33, 1056) but at higher values it gives no "inversion" for the yield of  $\text{NH}_3$ . The inversion easily found by Masted at high temp., is quantitatively attributed to a reversion of the  $\text{H}$  atoms formed at those high temps. with the  $\text{N}_2$  made in the reaction zone at about  $1800\text{--}1000^\circ$ , giving apparent but false high values for  $\text{NH}_3$  formed at high temps.

— 1 —

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8c

2-1

In the presence of water, the yield of  $\text{H}_2$  is increased to 27% (Acta Physico-Chim. URSS, 1937, 13, 100). The yield of  $\text{H}_2$  is also increased by the presence of  $\text{CO}_2$ ,  $\text{NO}_2$ ,  $\text{NO}$ , and  $\text{N}_2\text{O}_4$  contained in air (ibid., 1937, 13, 100). The yield of  $\text{H}_2$  is decreased by the presence of  $\text{SO}_2$  (ibid., 1937, 13, 100). This is explained by the action of the water on the catalyst, which increases the diameter of the vessel, allowing the diffusion of  $\text{H}_2$  contained in air to narrow vessels. It is known that the addition of  $\text{N}_2$ ,  $\text{NO}_2$ ,  $\text{CO}_2$ , and  $\text{NO}$  to the atmosphere with the same hydrogen requirements, does not increase the yield, and from the water-gas experiments it can be seen clearly with that case. From the last data, and it is believed that equilibrium is attained in the reaction, if  $\text{H}_2\text{O}$  is present initially  $\text{CH}_4 + \text{H}_2\text{O} \rightleftharpoons \text{CO} + 3\text{H}_2$ , and equilibrium is not attained, the reaction gives a suitable source of  $\text{H}_2$  for the  $\text{H}_2\text{O}-\text{CO}_2$  synthesis.

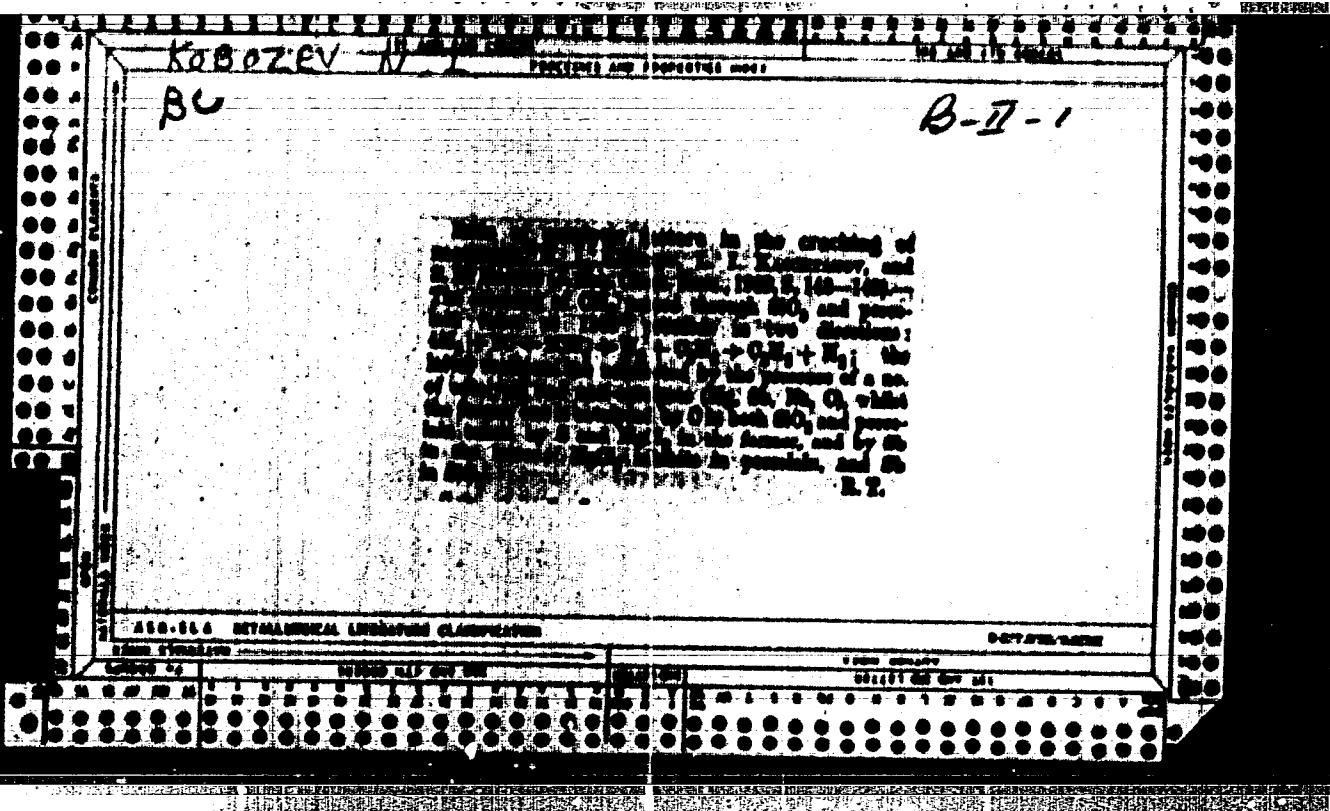
**412.14.4 METALLURGICAL LITERATURE CLASSIFICATION**

**APPROVED FOR RELEASE: 09/18/2001**

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BC

B-I-1

Preparation of hydrogen and hydrogen-nitrogen mixtures by the explosive oxidation of methane.  
M. I. Kozhevnikov, J. S. Karanayev, and L. I. Karachanov  
(J. Chem. Ind. Russ., 1966, 12, 1080-1086).—The product of explosion of 1:1 O<sub>2</sub>-CH<sub>4</sub> mixture contains equal vol. of CO and H<sub>2</sub>, and given, when converted, 2:22 vol. of H<sub>2</sub> per vol. of CH<sub>4</sub> taken. 1:1 N<sub>2</sub>-H<sub>2</sub> mixtures are obtained by performing the reaction with 3:1 O<sub>2</sub>-N<sub>2</sub> mixture, and the energy liberated by the explosion suffices for its prep. from nit. The composition of the reaction product corresponds to that which would be expected for the equilibrium mixture, on thermo-

CA

2

The hydrogeneration of aluminum nitride by active hydrogen. N. N. Mikhaylov, B. V. Kravtsov and V. M. Svetov. Sov. Pat. No. 104,111 U. R. S. S. [U.S.S.R.] 2,209,924 (1967) (in Russian).—Al nitride (made by heating AlN over powdered Al<sub>2</sub>O<sub>3</sub>-SiO<sub>2</sub> and water, 25-30% AlN) was placed in an U-shaped quartz discharge tube and H<sub>2</sub> or H<sub>2</sub> and N<sub>2</sub> (1:1) at 1-4 mm. pressure was passed over it while an ac. discharge of 0.05 amp. was passing through the tube. During the expt. the tube was kept in liquid air to prevent the NH<sub>3</sub> formed. In every case NH<sub>3</sub> was formed and at the same time an AlN<sub>x</sub> was formed that was at least partly volatile even in liquid air. Because of this the N content of the impure nitride increased during the expt. in spite of the NH<sub>3</sub> that was formed. It also prevented the formation of a coating of Al over the AlN that would stop the formation of NH<sub>3</sub>. The part. of NH<sub>3</sub> formed varied but in some cases amounted, in an hr., to about 10% of the N<sub>2</sub> in the AlN. The activated H was in the act. form because the hydrogeneration was most rapid when the discharge had the color of the spectrum line of H.

John H. Miller

450-114 METALLURGICAL LITERATURE CLASSIFICATION

*Sav**A 54  
w*

140. **Explosion Oxidation of Methane.** N. Kubasch, J. Kastnerovský and L. Kastnerovská. *Acta Physicochim. S. S. R.* 32, 107-119, 1956. *In German.*—The mechanism of  $\text{CH}_4$  oxidation which takes place in the explosion of equimolar mixtures of  $\text{CH}_4$  and  $\text{O}_2$  is investigated. The experiments are carried out in a bomb of the Berthelot type by means of a glowing tungsten wire. The initial and final pressure in the bomb are measured by a mercury manometer valid up to 4 atmospheres; and the resultant gases  $\text{CO}_2$ ,  $\text{CO}$ ,  $\text{C}_2\text{H}_4$ ,  $\text{C}_2\text{H}_6$  and  $\text{CO}$  are analyzed by the Krompel method. The influences of the following factors upon the explosive results are studied: pressure, the content in the initial mixture of  $\text{CH}_4$ ,  $\text{O}_2$ ,  $\text{N}_2$ ,  $\text{CO}_2$ ,  $\text{CO}$ ,  $\text{H}_2\text{O}$ ; and the diameter and condition of the walls of the explosive vessel. It is found that the final state of the system has to be established entirely from thermodynamical equilibrium conditions. This reaction gives mainly  $\text{CO}$  and  $\text{H}_2$ , and provides a simple and cheap process for the manufacture of  $\text{H}_2$  or of a mixture of  $\text{N}_2$  and  $\text{H}_2$ .  
H. H. Ha.

## A.I.D.-I.R. METALLURGICAL LITERATURE CLASSIFICATION

SIGHT-READ INDEX

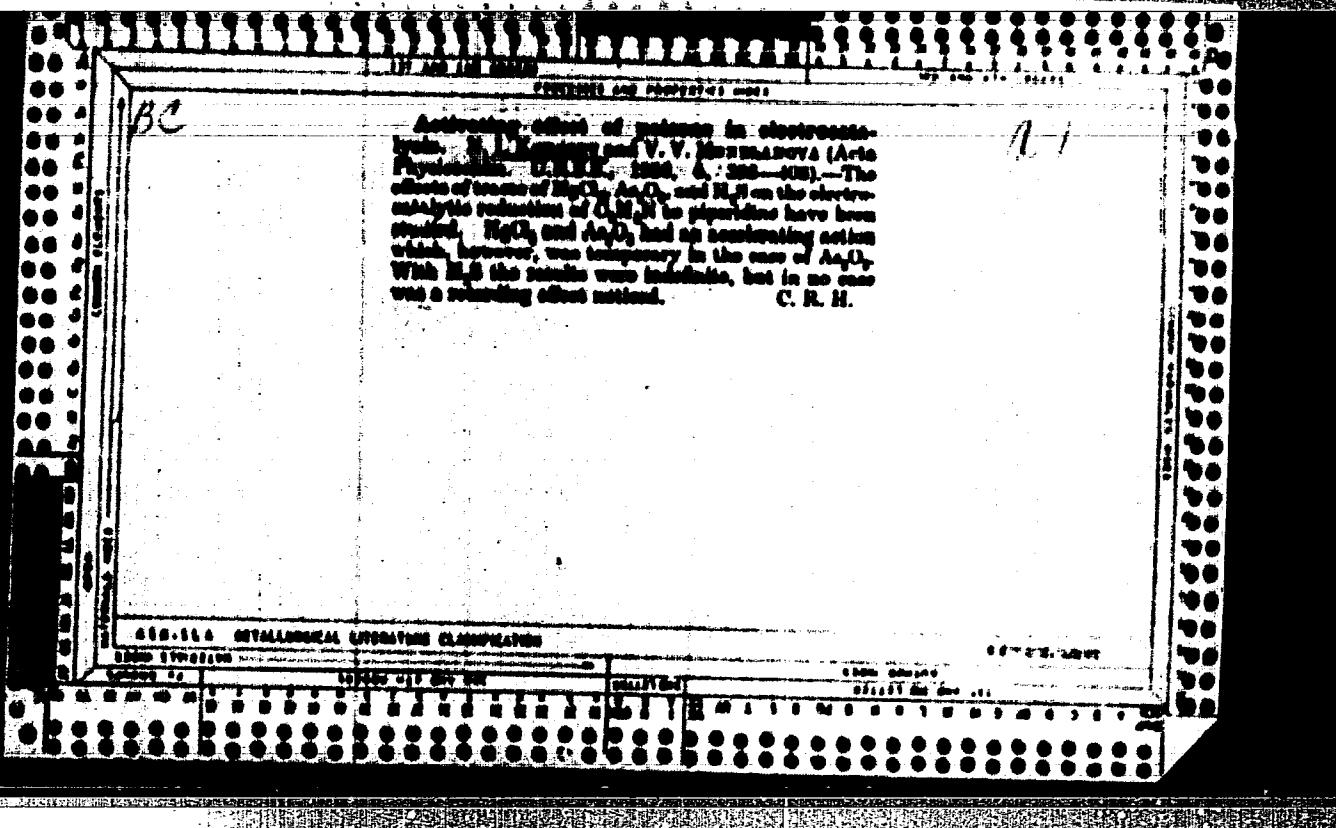
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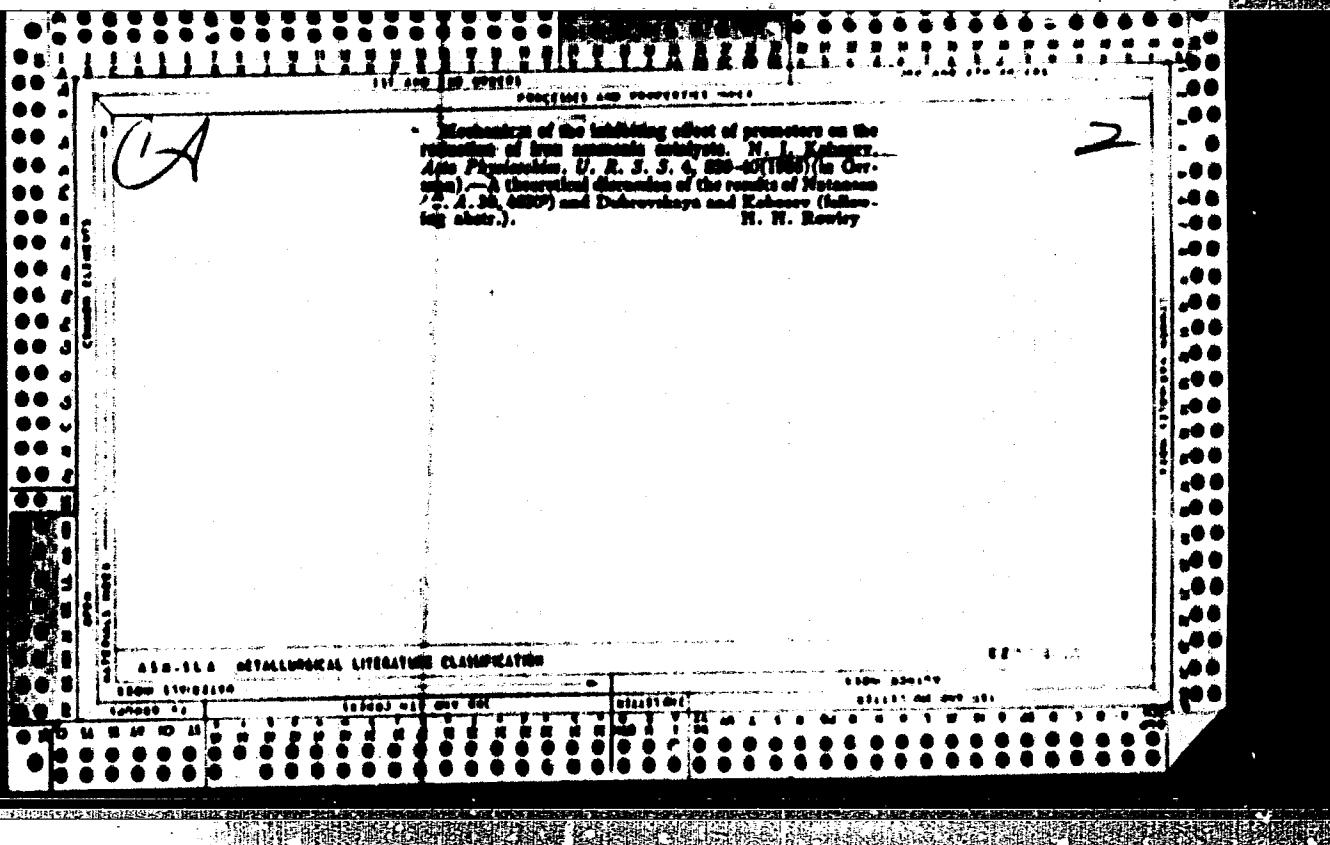
KOBZEV, N.I.

processes and properties)

The thermodynamics of endothermic processes of nitrogen fixation: N. I. Kobzev, B. S. Tsvetov and Ya. S. Esterovskii. *Acta Physicochim. U.R.S.S.* 6, 345-62 (1930) (in English). Yields and energy and material expenditures for the reactions  $N_2 + H_2 = 2NO$  (I),  $N_2 + 2CO = 2CO + 2NO$  (II),  $N_2 + 2C + H_2 = 2NH_2$  (III),  $N_2 + C_2H_4 = 2HCN$  (IV) and  $N_2 + C_2H_6 = 2HCN + NH_3$  (V) are summarized. Failure to consider side-reactions gives results much above the exp'd. yields, but much closer agreement is obtained when these are taken into account. I is the only feasible method for direct synthesis of NO and the most NO is lost. NO is the most valuable form of fixed N. Production in the glow discharge under special conditions requires 720 kWhr. It may be possible to decrease this in the cold glow discharge so that it could compete with XH<sub>4</sub> synthesis. II is not expedient because of the low yield and large amounts of energy and raw material consumed. The raw materials for III and IV are too expensive, but V gives only a slightly lower yield, the C<sub>2</sub>H<sub>6</sub> is cheap and the by-products, NH<sub>3</sub> and C<sub>2</sub>H<sub>2</sub>, are valuable.

K. R. Rushton





*Ca*

The adsorption properties of promoted iron oxide in relation to the distribution of the promoters in the oxide form of ammonia precipitate. A. Dovgopyan and N. I. Kachman. *Acta Physicochim. U. S. S. R.*, 34, 54-58 (1960) (in German).—The adsorption isotherms of  $O_2$  on pure  $Fe_2O_3$  and on  $Fe_2O_3$  which contained 10%  $Al_2O_3$  were studied. At  $-160^\circ$  and  $+400^\circ$ , X-ray photographs of  $Al_2O_3$  crystals heated to various temps. showed that the adsorbing power of  $Fe_2O_3$  decreased as the crystals became larger. The kinetics of  $O_2$  desorption from promoted and unpromoted  $Fe_2O_3$  studied at various temps., showed that the activation energy of desorption is independent of the presence of a promoter and averages 10,000 cal. Thus, even in the case of the promoted  $Fe_2O_3$ , the adsorption centers are the  $Fe_2O_3$  itself. It was found that the addition of 10%  $Al_2O_3$  to  $Fe_2O_3$  lowered the sp. adsorption of  $O_2$ . This proves that the dissolved  $Al_2O_3$  is strongly adsorbed on the surface of the  $Fe_2O_3$  crystals. From the data found, the equal const. between the dissolved and adsorbed  $Al_2O_3$  was used, and the following equation derived where  $a$  is the degree of shielding of the  $Fe_2O_3$  surface by adsorbed  $Al_2O_3$ ,  $r$  is the percentage by wt. of  $Al_2O_3$  and  $t$  is the av. length of one

and Mn 0.45% was subjected to dilatometric, micrograph, magnetic and hardness exams. Specimens quenched from  $1200^\circ$  were entirely austenitic. If reheated to  $710$  or  $870^\circ$  ppts. of carbides took place and upon slow cooling below  $140^\circ$  martensite was formed. Specimens which were cooled rapidly from  $1200^\circ$  to  $800^\circ$  or less or were quenched from  $1200^\circ$  and reheated to  $800^\circ$  or less and held at that temp. for 20 hrs. do not form martensite on cooling. Martensite forms only after ppts. of carbides.

H. W. Kachman

AIA-51A METALLURGICAL LITERATURE CLASSIFICATION  
SEARCH SPECIFICATION

82-178-48-02

SEARCHED	INDEXED	FILED	SEARCHED	INDEXED	FILED
1	2	3	4	5	6

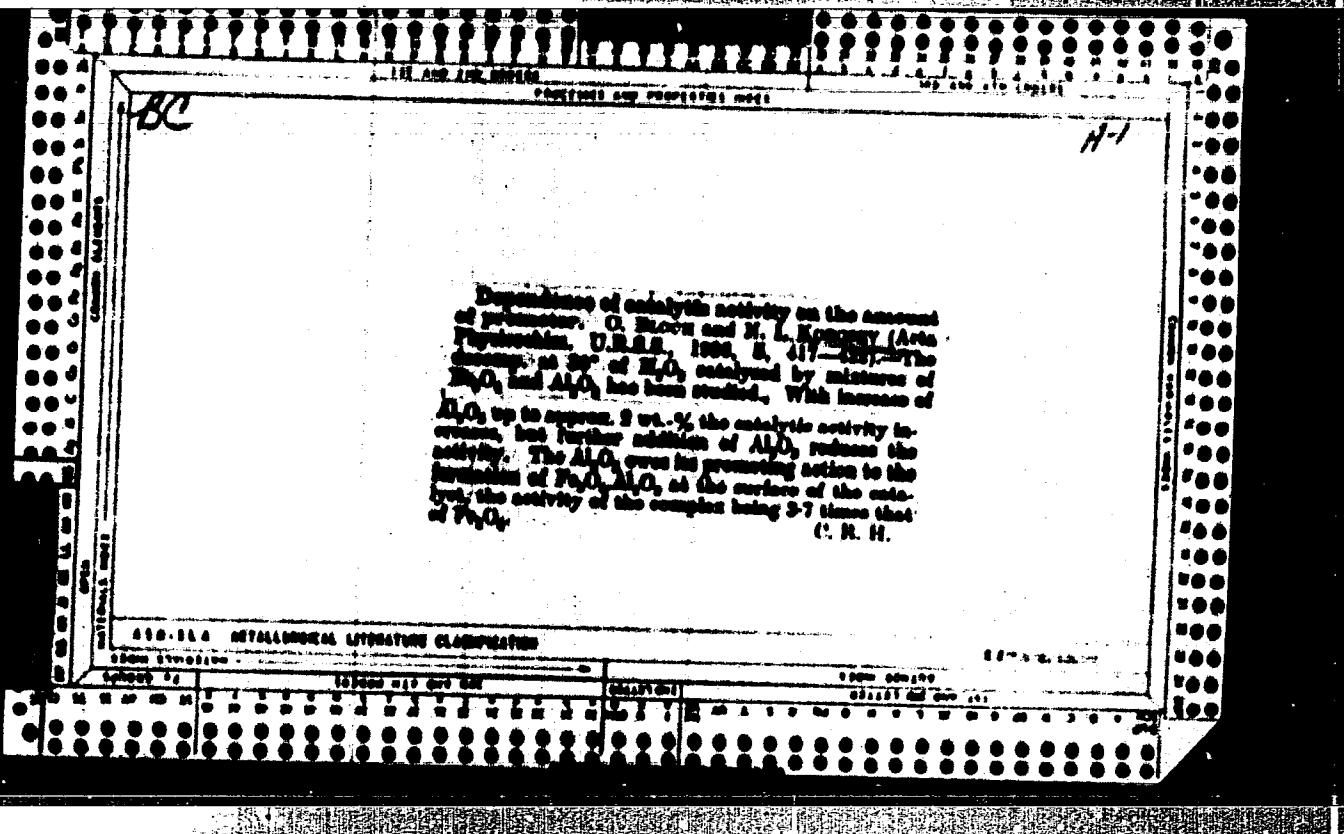
*Sov**A33**V*

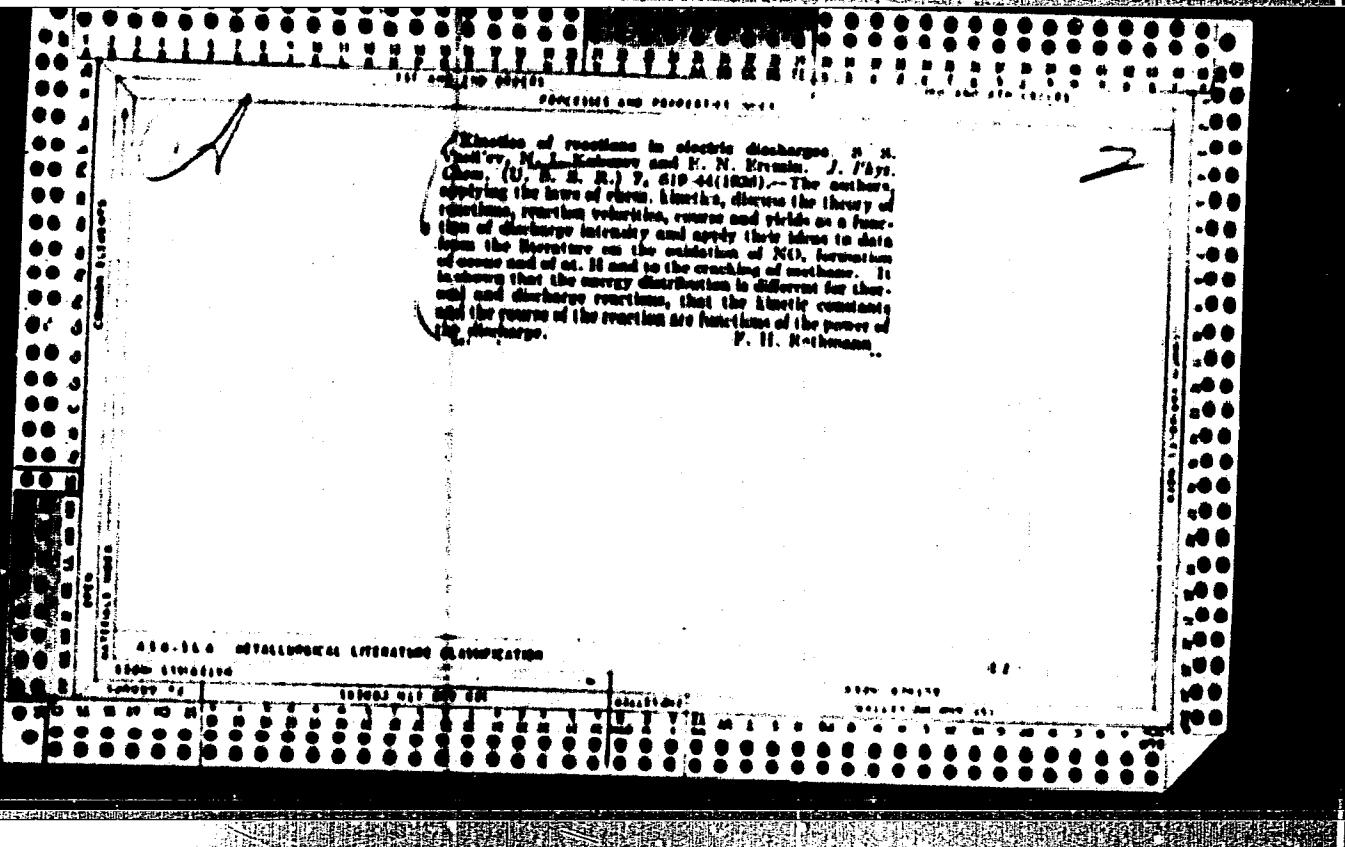
Electron Activation Viscosity in Discharges. S. S. Vinogradov, M. B. Kostyuk and B. N. Kravtsov. *Atomophysika*, No. 2, p. 24-29, 1958. In conclusion.—It is shown that the principle activation methods may be applied to reactions in the discharge. The kinetic schemes of the following reactions are determined and compared with the experimental data: Oxidation of nitrogen in the glow discharge, formation of ozone in the silent discharge, formation of atomic hydrogen, cracking of methane in the glow discharge. It is shown that the conditions of energy absorption during electrical activation are distinguished fundamentally from the conditions of thermal activation. In the above cases the kinetic constants are found to be invariant with respect to the change of velocity of passage of the gas through the discharge; they depend, however, on a whole series of other factors and above all on the work of discharge. It is also shown that when the parameter of the specific energy (the ratio of the work of discharge to the velocity of flow of the gas through the discharge) is introduced, it is possible to ascertain the influence of the work of discharge upon the velocity of the electrical activation process. The paper is replete with mathematical analysis, experimental data, diagrams and bibliography. H. H. Ha.

## A.I.A. METALLURGICAL LITERATURE CLASSIFICATION

KOBZOV, V. I.

Use of the Skin Effect in Investigating Thin Metal Layers. U. G. Gitter and N. J. Kostyev (*Acta Physicochim. U.S.S.R.*, 1936, 8, (2), 243-251 (in German); and *Zurnal Fizikal'noi Khimii* (*J. Phys. Chem.*), 1936, 8, (2), 206-223 (in Russian)).—Electrolytic films of iron on platinum and silver were studied by the method of high-frequency resistance measurement based on the skin effect. The change in high-frequency resistance depends on the change in the magnetic permeability ( $\mu$ ) of the film. The variation of  $\mu$  with the thickness of the layer, the current density during electrolysis, and time of aging after deposition are discussed in the light of Becker's theory of film structure (*Z. Physik*, 1930, 88, 283) and W. E. Lamb and W. E. Parry's data (*Met. Abstr.* (*J. Inst. Metals*), 1932, 86, 669). The method may be used for studying the kinetics of layer crystallization; thus in the formation of iron-platinum alloy on annealing the upper limit of the diffusion rate was found to be  $10^{-9}$  cm./second. Deposition of a zinc film on iron by electrolysis is accompanied by diffusion of zinc into the iron.—N. A.





Anticatalytic influence of anions in electrocatalysis.  
N. I. Vaynshteyn and V. V. Moshkovskaya, *J. Russ. Chem.*, 10 (1957), 1049-1051; *J. Russ. Chem. Soc.*, U. R. S. S. 4, 1957, No. 10, 1049-1051. An anion (I) was reduced to a hydride (II) by electrolytic cathodic reduction on a Ni electrode in 0.1 N HClO<sub>4</sub> solution. In the presence of anodic catalysis the yield of II increased. The yield of II decreased in the absence of anodic catalysis. The yield of II in the absence of anions is a linear function of the anion concentration, of  $1 \times 10^{-4}$  to  $1 \times 10^{-3}$  moles per liter, and the reaction c. d.,  $HgCl_2$  dissolved and triple the yield of II for a given c. d., the relative effect of different anions on the yield of II is as follows: c. d., the relative effect of different anions on the yield of II is as follows:  $Cl^- > F^- > Br^- > I^-$ . Similarly the anode potential of the reduction of anions decreases. For example, the anode potential of the reduction of  $Cl^-$  is -0.45 v. The small current density of the reduction of  $Cl^-$  (100 mA/cm<sup>2</sup>) at the anode potential of  $-0.45 \pm 10^{-3}$  moles). At the same time  $Ag^+$  the potential of which may be changed from  $-0.1$  to  $-0.2$  mole.  $Ag^+$  per liter at the same potential of  $-0.45$  v. which undergoes no II whatever is produced. The results are much simplified. F. H. R.

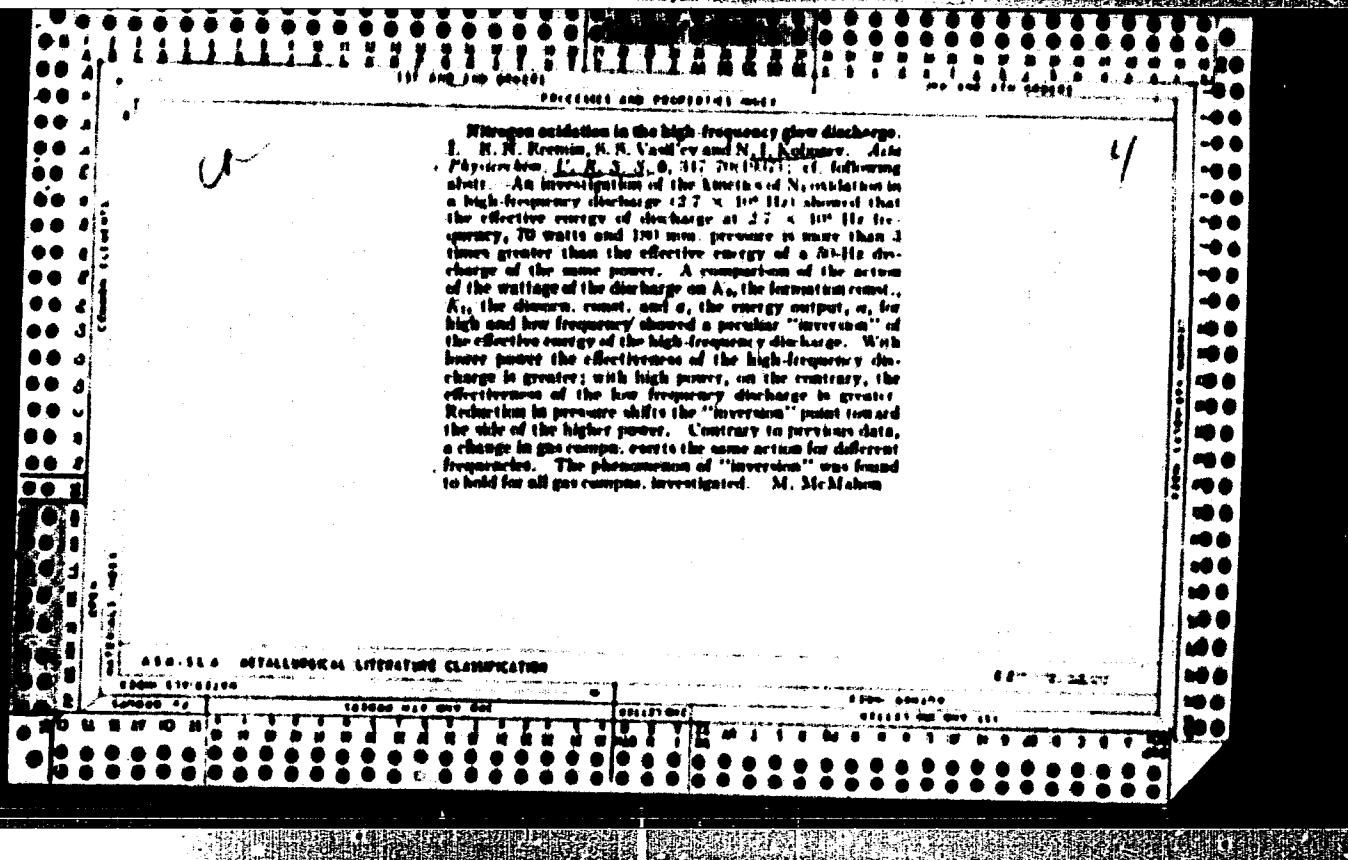
*dx*

*18*

The mechanism of the retarding effect of promoters on  
the reduction of iron-cyanide oxydote. N. I. Katsenay  
*J. Phys. Chem. U.S.S.R.* 8, 226-33 (1937); *V. C. A.*  
20, 7007. Data are given for the retarding effects of  
K<sub>2</sub>O, BaO, KP and Al<sub>2</sub>O<sub>3</sub> on the reduction of Fe<sub>3</sub>O<sub>4</sub> by  
H<sub>2</sub> and of MgO on that of FeO. Promoter action of the  
catalyst results when the added substance is surface-  
active and reduces the rate of reduction of the iron oxide.  
P. H. Kethmann

450-114 METALLURGICAL LITERATURE CLASSIFICATION

ca  
2  
The two nature of the relation of the catalytic activity  
to the composition of the promoter. O. I. Nikish and  
N. V. Kabanov. *J. Phys. Chem. (U. S. S. R.)* 6, 363 (1932).--The reaction of  $\text{Al}_2\text{O}_3$  in  $\text{Fe}_2\text{O}_3$ -lattice catalysts  
is discussed.  
P. H. Rathmann



## RECORDED AND INDEXED BY [initials]

Nitrogen oxidation in a high frequency glow discharge  
H. H. N. Pernau, N. S. Vaidya and N. J. Buddeau  
*J. Phys. Chem.* 61, 188-190, 1957; cf. preceding abstract.  
At lower 20 to 100 mm. pressure and 70 w., a  
high-frequency ( $3.7 \times 10^4$  Hz) discharge is 3 times as  
efficient as a 50-Hz discharge. Above 90 w., the  
low-frequency discharge is the more effective. A com-

pilation of the effects of  $3.7 \times$ ,  $5 \times$ ,  $7 \times$  and  $10 \times 10^4$  Hz<sup>-1</sup>  
frequencies shows that the effect is the same in all cases  
and hence not due to chem. resonance effects. No differ-  
ence in effect was observed when either internal or  
external electrodes were used. At higher wattages the  
max. yield is obtained at higher relative concn. of O<sub>2</sub>.  
Electron temp. as detd. from the spectra of the dis-  
charges is higher at 70 w. high frequency than at low  
frequency and is higher at low voltage than at high  
voltage, and higher at low pressure than at high pressure.  
F. H. Mathmann

## 410-114 METALLURGICAL LITERATURE CLASSIFICATION

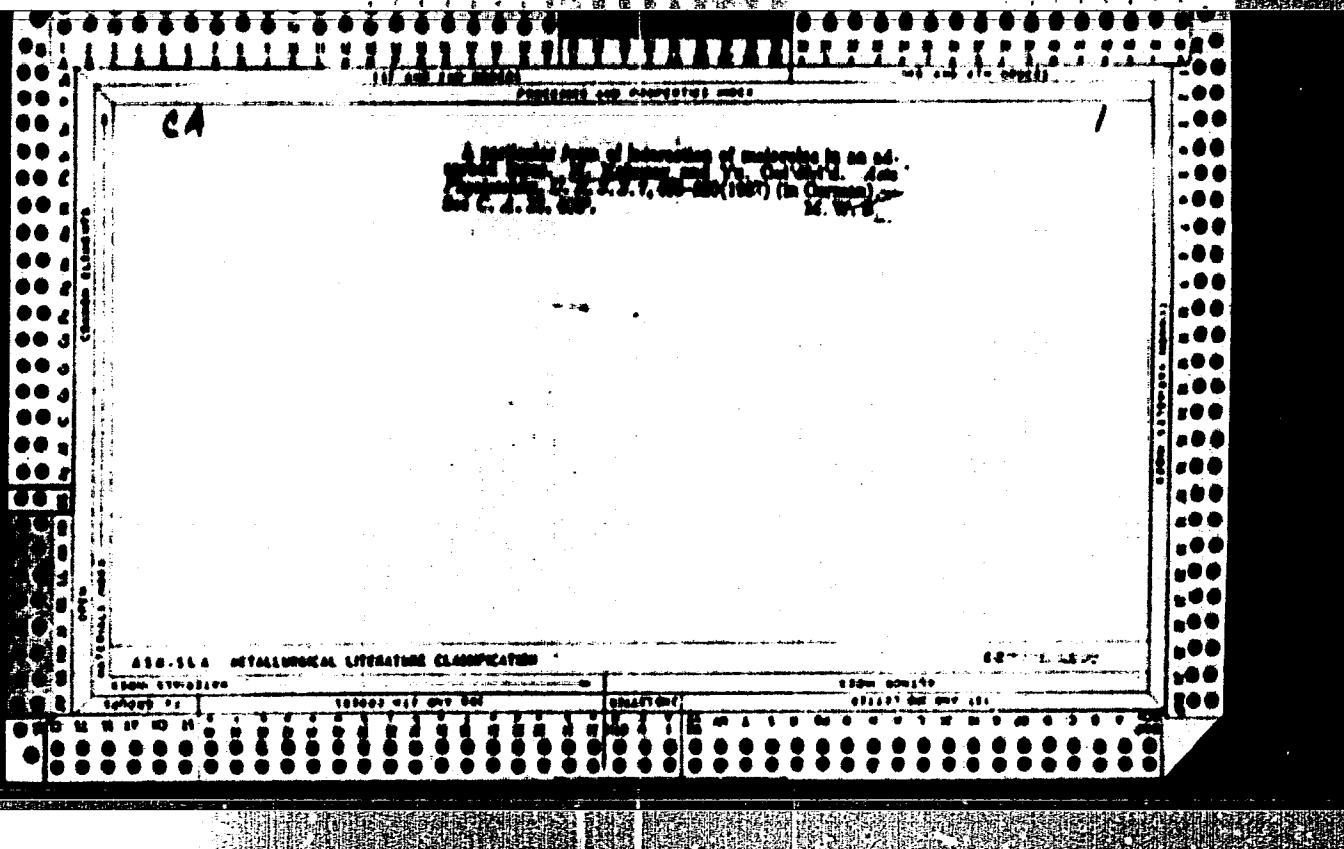
SEARCHED

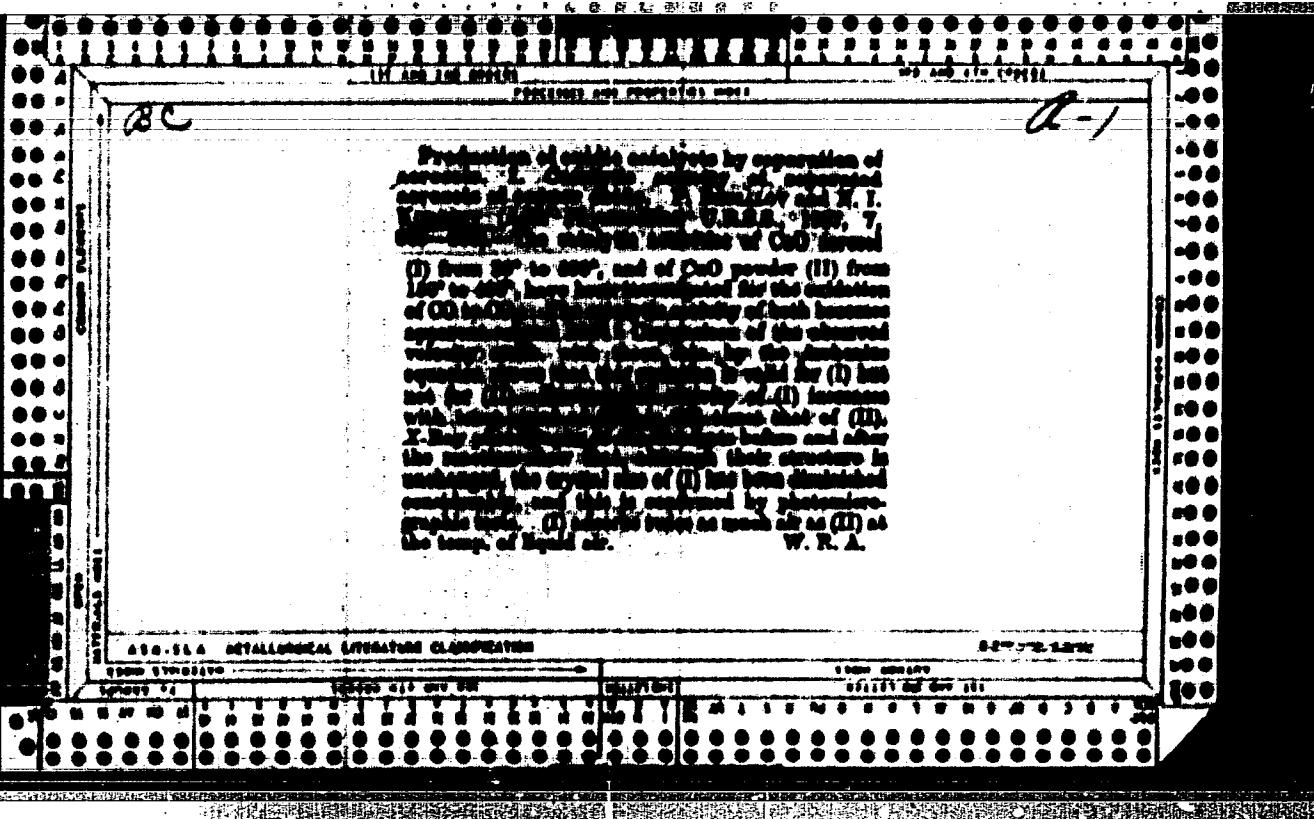
INDEXED

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"APPROVED FOR RELEASE: 09/18/2001

CIA-RDP86-00513R000723410014-9

X  
Influence of the current density on the yield of acetone  
in electrical cracking of methane. N. S. Vasil'ev,  
K. A. Kabanov and N. M. Kravtsov. Akad. Nauk SSSR  
1976 No 19871. A criticism of the above paper  
A. A. Pogorelyy

APPROVED FOR RELEASE: 09/18/2001

CIA-RDP86-00513R000723410014-9"

B/C

A-1

Preparation of carbon catalyst by deposition of aerosols. II. Intermediate compounds in the catalytic oxidation of carbon monoxide on ferric oxide. K. Ivanov and N. Kostyuk. (J. Phys. Chem. Russ. 1959, 3, 1-17).—The reaction  $2CO + O_2 \rightarrow 2CO_2$  is of zero order on a  $Fe_2O_3$  aerosol at 400°, and of the first order at 500—550°. It is of the first order on ordinary  $Fe_2O_3$  powder at all temp. The activation energy is the same in both cases (9.15 kg.-cal.). Strong sorption of CO (up to 1.3 mole per mol. of  $Fe_2O_3$ ) occurs during the reaction. The activation energy of sorption is 4.45 kg.-cal. on the  $Fe_2O_3$  powder and 5.04 kg.-cal. on the aerosol. Results can be explained by the assumption of the existence of intermediate compounds  $(Fe_2O_3)_{x,y}CO$ , with  $x:y > 2:2$ . K. R.

## A10-116 METALLURGICAL LITERATURE CLASSIFICATION

8-8-1972 10:27 AM

11 AND 128 Dots

FILM 100% PROTECTED

B6 RY

Preparation of cobalt catalyst by deposition of  
alcohol. I. Catalytic activity of copper oxide  
deposited from an alcohol. «P. Basalov and  
N. Korotov. J. Phys. Chem. Russ., 1957, 3, 815—  
827.» Commercially active CuO was obtained from  
an aerosol and its activity in oxidizing CO has been  
investigated at 200—400°. The oxidation begins at 200°  
< with an ordinary CuO powder. The reaction  
velocity follows the standard Arrhenius' law (activation  
energy 35.2 kg.-cal.). Activity of the aerosol increases  
with temp.; at 300° it is 700 times as active as the  
CuO powder. X-Ray photographs and photomicro-  
graphs show that the aerosol has the same structure  
as the powder, but smaller crystallites, which  
decrease further after catalysis. The aerosol absorbs  
twice as much air as the CuO powder, and 2.5 times  
as much after catalysis.

K. R.

410-114 DETACHMENT LITERATURE CLASSIFICATION

6-47-1000-100

1000-1000-100

1. Preparation of oxide catalysts by precipitation of zero-valent Fe. The formation of magnetite compounds during the catalytic oxidation of carbon monoxide on iron oxide. Z. Tsvetov and N. Kachman. *J. Phys. Chem.* (U.S.S.R.) 51, 1-17 (1947). On a powdered  $\text{Fe}_3\text{O}_4$  catalyst at 300-400° the  $\text{CO} \rightarrow \text{CO}_2$  oxidation obeys a nearly parabolic kinetic equation, while on powder at 120° to 400° it obeys a first-order equation. On both catalysts the activation energy is  $E = 3130$  cal., while  $K_0 \ln K = \log K_0 - E/RT$  is 4.14 for aerosol and 3.98 for the powder. Z.

X-ray and photomicrographic studies of both catalysts show that during the catalysis an intense process of crystal structure reconstruction takes place so that the crystal grain size is completely altered. The cubic aerosol crystals of  $10^{-4}$  cm. change to rhombohedral of  $10^{-1}$ , while the rhombohedral  $\text{Fe}_3\text{O}_4$  powder of  $10^{-4}$  cm. grain size recrystallizes in the same system to a size of  $10^{-1}$  cm. The effect of heating the powder to 1100° is the same as the process of catalytic reduction.  $\text{CO}$  is so strongly adsorbed by  $\text{Fe}_3\text{O}_4$  that definite stoichiometric interphase compound formation of an oxyferricyanide type must be assumed. The adsorption may also be considered as an activated adsorption with  $E = 4480$  cal. for the powder and 3040 cal. for the aerosol. The mechanism of the  $\text{CO} \rightarrow \text{CO}_2$  oxidation tends to be assumed to involve the  $(\text{Fe}_3\text{O}_4)(\text{CO})_x$  adsorption phase on a direct link. Z. H. Kachman

CA

A particular form of interaction of molecules is an adsorbed layer. N. Kabanov and Yu. Gribnikov. *J. Phys. Chem. (U. S. S. R.)* 10, 244-72 (1957).—Theoretical analysis. It is assumed that the most typical case is that where, given the adsorption potential around the adsorbed molecule, it is lowered. The resulting polarization of the surface molecule's attractive forces greater than the polarization-interaction of the molecule, and in fact, deviations from the VdW equation for the liquid state of a two-dimensional gas, is increased there, potential rapidly rising with the extent of surface covering, desorption of the adsorption molecule with slower rate of desorption relative to coverage, and in desorption of adsorption from the unbound, low and a lowering of the energy of activation the more the surface is covered. Empirical data on the description of propylene from G. et al. 220-237°K, confirm these predictions as according to the theory of active centers. P. H. Rothman.

*WA*

2

The activation process during reactions in electric discharges. I. A. I. Kabanov, N. S. Vinogradov and R. N. Braverman. J. Phys. Chem. U.S.S.R. 19, 243-277 (1937).—Theoretical and mathematical. The nature and use of the energy of elec. activation, the nature of the active mode presented, the kinetics of "elec. catalysis," the probability of energy transfer by "collisions of the second kind" as based on spectroscopic studies of nitrogen oxidation in an elec. discharge, are considered from the point of view of elucidating the relations between the rate of reaction, intermediate elementary processes, and the energy balance of the discharge. The rapid. data available indicate that theories based on loss of the active intermediate agents are not tenable; a mechanism involving polarizing excited mode, similar to active mode, is proposed. The difference between elec. and thermal catalysis and activation is that in the former dissociation energy dissipation does not exist, activation catalysis taking place by energy transfers by "collisions of the second kind" between normal mode, and recombining ions and electron-excited mode.

P. H. Kabanov

## AIAA METALLURGICAL LITERATURE CLASSIFICATION

1960-1970

1970-1979

1980-1989

1990-1999

KOBOZEY, V.I.

The electrolytic oxidation of ammonia to ammonium nitrate. N. J. Kobozev, T. V. Moshkareva and A. L. Shcherbinin. *J. Russ. Acad. Nauk. (U.S.S.R.)* 10, 1307-13 (1962). NH<sub>3</sub> is best oxidized can be made in a 2 compartment cell. The anode is a carbon (95% carbon, 5% MnO<sub>2</sub>) (1/4" x 1/2") (1000 ml) as a catalyst. The cathode is 100% K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub>. A 2 mm side stone stopper gives best results. The c. i. has little effect on the reaction. NH<sub>3</sub> is passed into the anode compartment during the reaction to reduce evolution of CO<sub>2</sub> and keep the pH at about 8.42. About 75% of the NH<sub>3</sub> is oxidized to NH<sub>4</sub>NO<sub>3</sub>.

CO

2

A theory of the formation of catalytically active "nanoclusters" on surfaces. I. M. Kabanov, *Zhur. Fiz. Khim.*, **U. S. S. R.**, **3**, 6, 606-611 (1969) (in Russian).—Assuming that the active center of the catalytic capacity is an amorphous (disordered) phase organized into sub-units obeying the laws of d. fluctuation, A. developed a theory that explains the optimum activity for the nature, dispersion, and form, of pores, and for the choice of promoters and the order of introduction of the functioning substances. The crystal carrier data, only the no., but not the properties, of the nanoclusters. An equation is given for the max. activities of two catalysts. This equation helps to account for the change in the order of catalytic reactions. Cf. Kabanov and Neimanov, *C. A.*, **64**, 14802, II. An application of the theory to the synthesis of ammonia and to the catalytic and electrocatalytic hydrogenation of the ethylene bond. N. J. Kabanov and I. I. Gavchik-Ovrichik, *Zhur.*, **14**, 1-24 (1969) (in Russian).—On the basis of their own exp. data as well as that from other authors and using the equation previously derived (cf. preceding abstr.) I. I. and K.-O. note the av. no. of atoms in active nanoclusters to be 2 Pt for the reaction  $N_2 + 3H_2 = 2NH_3$  (cf. K.-O. and K.J.) 3 Pt for  $H_2 + O_2 = H_2O$  (cf. Danilov and Kucheria, *C. A.*, **59**, 6007).

and 6410); 2 Pt for formic acid hydrogenation (cf. Schmitzsch and Zimmerman, *C. A.*, **54**, 3887); 4 Pt or 4 Ni for  $C_6H_6 + H_2 = C_6H_5$  (cf. Danilov, *C. A.*, **57**, 2020); 2 Pt or 2 Pt for the electrocatalytic hydrogenation of citric acid (according to Moshkina, Kabanov and Pleshovskii) in the presence of traces of  $HgCl_2$  and  $K_2AlCl_4$  catalyst polymer as activators. For reactions of  $H_2$  with disord. meth., the nanoclusters contain 2 atoms, for addts. to the C=C bond they probably contain 2-4 atoms. The protecting action of  $Fe_2O_3$  in synthetic ammonia catalyst is explained as a result of the preventing three-atom iron coordination in  $Fe_2O_3$  that of  $Al_2O_3$  to a protecting action against melting or evapn. of the nanoclusters. V. H. Rothman

## A10-150 RETAILORIAL LITERATURE CLASSIFICATION

64-14714-A0014

Activation process in reactions to electric discharges.  
II. N. J. Kolosov, B. B. Vasil'ev and R. N. Krasum. *J. Phys. Chem.* (U.S.S.R.) 11, 45-60 (1957); cf. *C. A.* 52, 4671. Oxidation of  $N_2$  is discussed. The elec. energy supplied to the discharge app. is chiefly spent in (a) heating the electrodes, (b) light emission by excited atoms, (c) inductive excitation of  $D_{\alpha}$ , and in (d) deactivation of active  $N_2$  mole.; the remaining energy (e) is used for NO synthesis. The energy loss (a) explains the increase of the yield of NO per erg supplied with increasing distance between the electrodes. The loss (c) is partly responsible for the dependence of the NO yield on the ratio  $c_{NO}/c_{O_2}$ ; at  $O_2$  excess,  $N_2$ , the yield increasing with that ratio at high c. d., and high pressure and decreasing with it at low c. d., and low pressure. Calculation of the energy (e) shows that the activation energy has a normal value; hence the active mode, to the discharge arc of the same kind as those in thermal reactions. B. C. P. A.

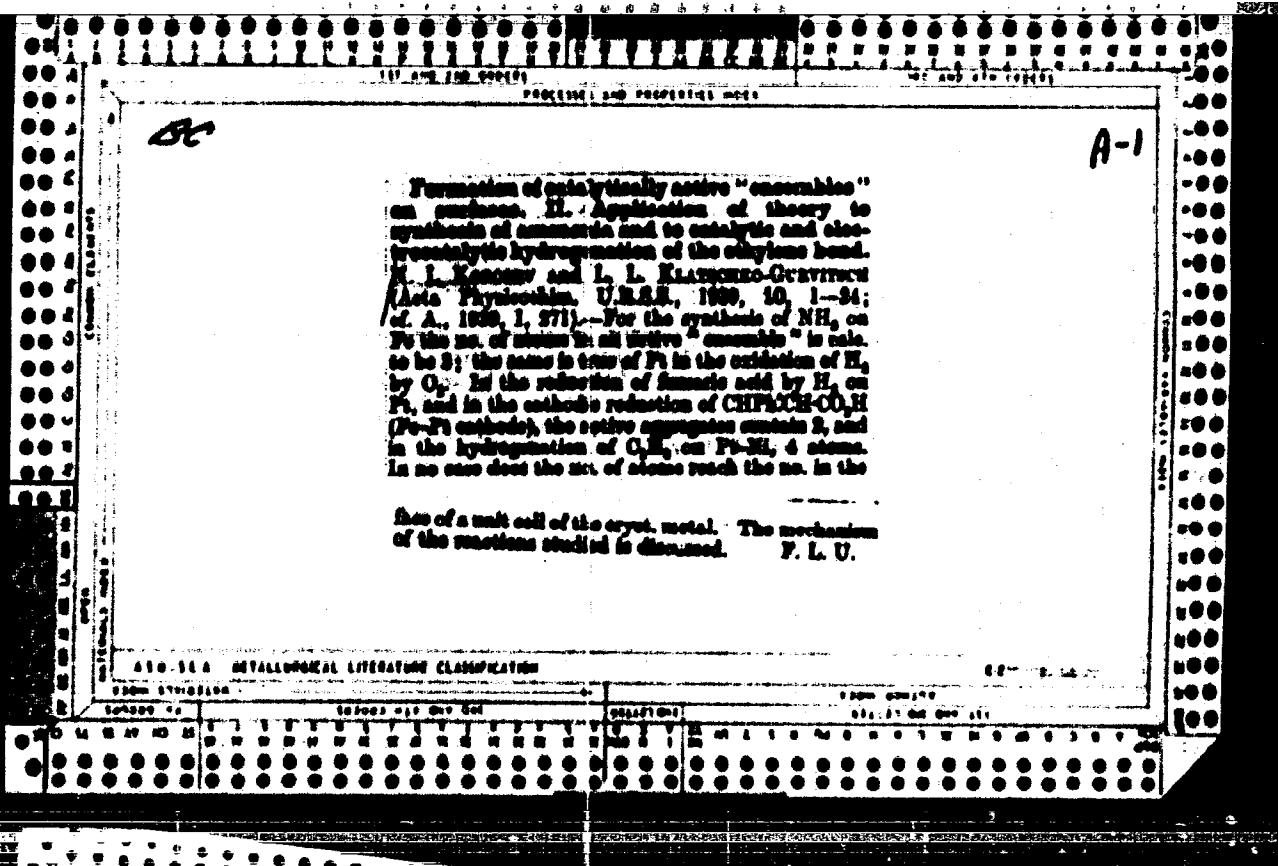
A correction to the article "Activation process during  
reactions in electric discharges," N. J. Antonov, N. N.  
Yudilev and N. N. Yermakov, *J. Phys. Chem.* (USSR) 11,  
11, 2020 (1957); cf. C. A. 51, 6067, 1957. The value of  
the spectrum appearing during the oxidation of H should  
be corrected to read: "To the activation energy of 1 e.v.  
corresponds the wave length 12,380 Å. The continuous  
spectrum found during the slow oxidation of H is ob-  
tained at 200 mm. Hg into the region of 5000-6000 Å.  
wave lengths." After a further discussion K., V. and  
N. come to the conclusion that the difference between the  
full activation energy of H molecules, read from the wave  
lengths of the continuous spectrum, and the energy trans-  
ferred during the oxidation of "the second kind" can be  
regarded as the thermal energy of activation which spans  
say 200 in the Stokes from  $4.37 \times 0.2 = 1.17$  e.v. = 21,700  
cm./mol. to  $8.00 \times 0.08 = 0.31$  e.v. = 600 cm./mol.  
W. H. Bratt

*Effect of reaction with the decomposition of solid catalysts.* In continuation of the previous communication of this subject by the presenters, L. B. V. Kudryavtsev, Yu. V. Kravchenko, A. N. Goryainov and N. V. Tsvetkov, *J. Russ. Chem. (U.S.S.R.)* 11, 189-200 (1958) (cf. C. A., 51, 1975).—Data on the hydrodeposition by Ni on MgO in the temperature range from 300 to 500° at 3 different heat treatment temperatures roughly to the constant  $P_{H_2}$  and  $P_{H_2}$  were presented (as well  $P_{(CO)}$ , 0.01 atm) showing the course of the temperature reaction is indicated by the reduced the hydrogen content,  $H/P$ ,  $H/P$  or  $H/M$  in  $P_{H_2}$ .  $\beta$  is the degree of conversion,  $\alpha$  and  $\gamma$  are ( $N$  = part. of reduction reaction),  $\beta$  and  $\gamma$  are constants. The expression of  $\alpha$ ,  $\beta$ ,  $\gamma$  and  $\delta$  indicates, respectively, reaction; for  $\beta$ , nonselectivity on the edges of all directions symmetric or nonsymmetric on the edges of all crystals; for  $\beta$ , nonselectivity on the edges of all nonsymmetric where  $H/P = \text{const.}$ ; and for  $\beta$ , nonselectivity at distinct points of the individual crystal of the reaction. In the reduction of the oxidation of two (1) ( $Pd/H_2$ , unconverted), (2) ( $Pd/H_2$  prepared by  $0.1\% Al_2O_3$ ), (3) ( $Pd/H_2$  prepared by  $0.1\% Al_2O_3 + 0.1\% MgO$ ) or (4) ( $Pd/H_2$  prepared by  $0.1\% Al_2O_3 + 0.1\% MgO$ ) the conversion of the metal, determined by the thermodynamically derived expression indicates that the reaction is limited on the crystal edges. In (2) ( $Pd/H_2 + 1.5\% Al_2O_3$ ) and (3) ( $Pd/H_2$  not prepared), the reduction occurs on both of individual points on the polyhedral crystal surface. For (4) ( $Pd/H_2 + 1.5\% Al_2O_3$ ) the course of the reaction. From these data it is evident that catalysts do not have the same effect on the reaction mechanism of the reduction process as the reaction conditions.

*Effect of reaction with the decomposition of solid catalysts.* Cf. Bennett and Love, C. A., 58, 1975. —*Investigation of the kinetics of reduction of iron oxides.* 3. *J. Ind. 300-304 (1958).*—With the same procedure used in the preceding paper, the probability of initiation of the reaction and the linear rate of the propagation were determined. While Al<sub>2</sub>O<sub>3</sub> shows no specific and marked effect on the hydrodeposition process, K<sub>2</sub>O shows a strong neg. effect. The pos. catalytic effect of K<sub>2</sub>O in  $0.1M_2O-0.1M_3$  promoters to  $NH_3$  evolution is due to a reduction by the K<sub>2</sub>O of the otherwise inactive Mg carbonyl edge. The energy of activation is the same for the crystal faces, edges and polyhedral regions, and is about 17,000 cal. The net catalytic effect of the solid products is due only to the  $\beta$ -catalyzing certain basic hydrocarbons effects. The order of reactivity of the N atoms decreases in the order of hexagonal, polyhedral edges, edges and basal planes. IV. *The thermal decomposition of mercury oxides.* B. V. Kudryavtsev and E. S. Tsvetova, *J. Ind. 305-306.*—*Report: data are given on the thermal decompos. of mercury oxide at 400-600° on and in the presence of Na acetate or Na<sub>2</sub>O<sub>2</sub>.* The decomps. begins on the crystal edges and is accompanied with an energy of activation of 67,000 cal, while the reaction of differently prep. samples varies by a factor of 20. While "normal" mercury obtained by the action of Na acetate or of Na<sub>2</sub>O<sub>2</sub> on MgO catalyzes the reaction, apparently by its effect on the atoms of the MgO, which according to the mercury has no effect. The results indicate that the Volmer theory of competitive chem. reactions is not applicable. P. H. Rathenau

*BC**Q-1*

Volumetric and surface processes in the oxidation of nitrogen in glow discharge. I. R. A. Kozhevnikova and N. I. Kapustin. *J. Phys. Chem. Russ.*, 1958, 12, 551-559. At a pressure of 4 mm. Hg the rate of oxidation of dry  $N_2$  by  $O_3$  shows a max. at 50%  $N_2$ .  $H_2O$  decreases the rate between 40 and 90% of  $N_2$  and increases it at other ( $N_2$ ): 2% of  $H_2O$  is as active as 1%.  $CH_4$  inhibits the reaction  $>$  and  $NH_3$  and  $H_2$  <  $H_2O$ . An increase of the solid surfaces (quartz, glass, Al wire) accelerates the oxidation, especially in the presence of  $H_2O$ . It is supposed that NO is produced partly on the walls, this part of the reaction being inhibited by dipole moments, and partly in space.  $H_2O$  or  $NH_3$  does not affect the latter part since they do not alter the emission spectrum of the discharge. J. J. B.



R-1

Volume and surface processes during the oxidation of nitrogen by a glow discharge. I. B. A. KUROVALOVA and N. L. Kuznetsov (Acta Physicochim. U.R.S.S., 1939, 15, 681-683; cf. A., 1939, 1, 480).— The process is a combination of a vol. and a wall process, the latter being poisoned by polar molecules. The investigation of the effect of polar molecules thus provides a method of separating the two processes. At low pressures 80% of the NO is produced by the wall process. Toxic molecules do not affect the spectrum of  $N_2$ . Activating molecules, such as CO and  $CO_2$ , affect the spectrum and therefore influence the vol. process. The dissociation of NO in the discharge is not poisoned by  $H_2O$ , and hence is not a wall reaction. The results differ from those of Westhaven et al. (A., 1939, 683), the differences being explained.

A. J. M.

AD-A-114 METALLURGICAL LITERATURE CLASSIFICATION

111 422 222 00001  
PROC 11401 AND 19001 0141 0001

A.1

Volume and surface processes during the oxidation of nitrogen in a glow discharge. II. B. A. Korovatova and N. I. Krasnov (Acta Physicochim. U.R.S.S., 1938, 10, 613-634; cf. A., 1938, 1, 469).—The wall catalytic process occurring during the oxidation of  $N_2$  in a glow discharge is probably a reaction of  $N_2^+$  ions with adsorbed  $O_2^-$  ions, and at very low pressures the electrical oxidation of  $N_2$  is wholly due to this reaction.  $\cdot H_2O$  vapour poisons the wall process, but also has a positive catalytic effect on the vol. reaction in the gas space, especially in the  $O_2$  region. Addition of  $CO$  and  $(CO)_2$  to the gas produces an activating effect on the vol. reaction which is clearly reflected in the emission spectrum of the discharge.

O. J. T.

APPROVED FOR RELEASE: 09/18/2001 CIA-RDP86-00513R000723410014-9"

CA

4

Activation process and the nature of the active centers  
in oligopeptide hydroperoxides. V. V. Minkinova,  
N. I. Kozhevnikova and P. Filippovich. *Acta Physicochim.*  
*U. R. S. S. R.* 11, 617-43 (1939) (in English).--See C. A. 34,  
1229P. F. H. Rathmann

A10-914 METALLURGICAL LITERATURE CLASSIFICATION

RUDENKO, VLADIMIR VASIL'EVICH

"A Theory of the Formation of Catalytic Active Groupings on Surfaces --II. The Application of the Theory to the Synthesis of Ammonia and the Catalytic and Electrocatalytic Hydrogenation of the Ethylene Bond"; Zhur. Fiz. Khim., 12, No. 1, 1939. Moscow State University, Laboratory of Inorganic Catalysis. Red. 29 May 1938.

Report U-1613, 3 Jan. 1952

BC

A-1

Volume and surface processes in the oxidation  
of nitrogen in the glow discharge. II. R. A.  
Konovalova and N. I. Kozeev (J. Phys. Chem.  
Bull., 1959, 13, 286-300).—The part of the formation  
of NO taking place at the surface is presumably due to  
a reaction between  $N_2^+$  and adsorbed  $O_2^-$  ions.  
The relation between the rate of this surface reaction  
and the size of the reaction vessel is similar to that  
between the size of the vessel and the rate of re-  
combination of ions as determined by the min. dis-  
charge potential. In mixtures containing much  $O_2$ ,  
 $H_2O$  and  $NH_3$  increase the yield of NO; this is  
presumably due to oxidation of  $N_2^+$  by  $H_2O$  and,  
respectively, to oxidation of  $NH_3$ . (U and  $CO_2$  also  
raise the yield of NO. (V. A., 1959 I, 400.)

J. J. B.

I. A. Draganis,  
catalysis  
Moscow State U.

ATB-114 METALLURGICAL LITERATURE CLASSIFICATION

ITEM 110-0174	ITEM 110-0175	ITEM 110-0176	ITEM 110-0177
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CA

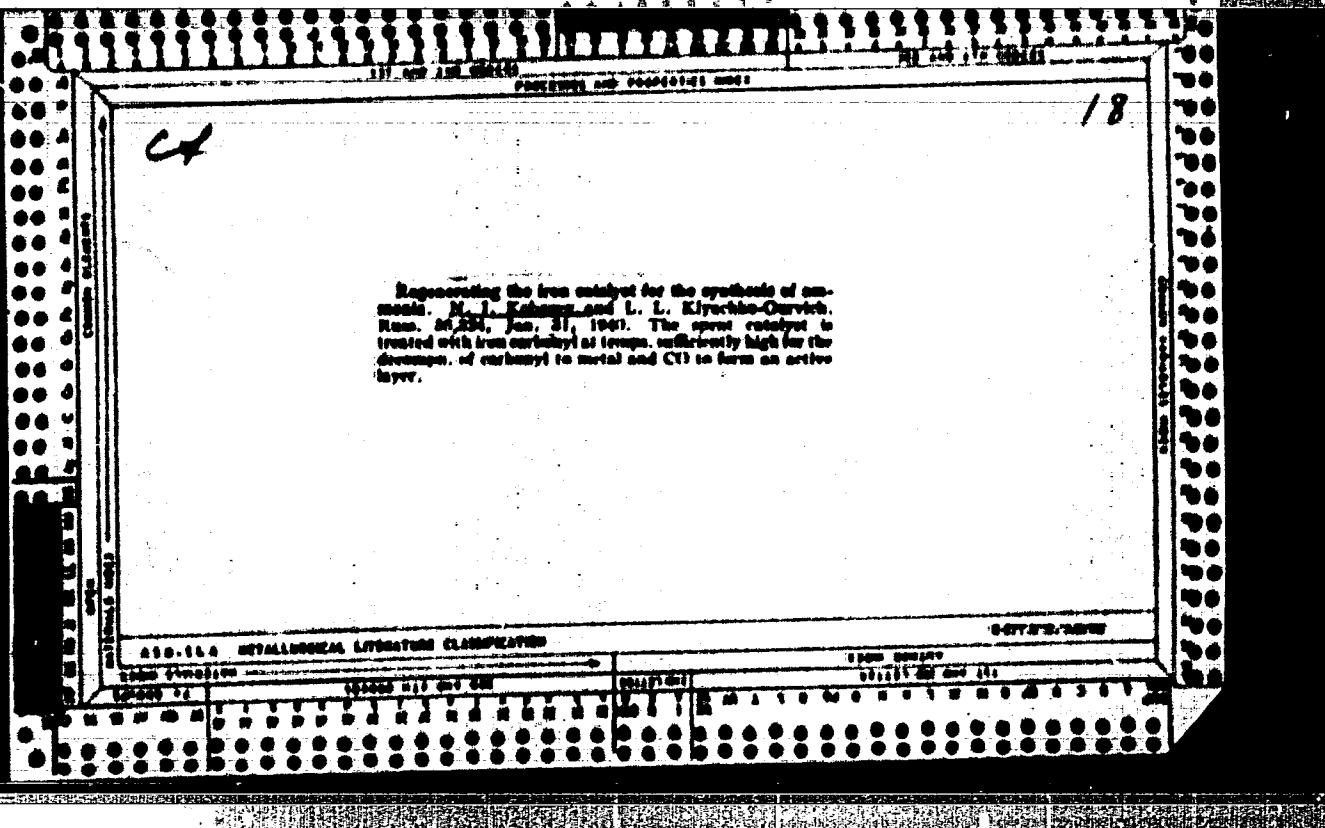
Activation procedures and the nature of the active centers in electrocatalytic hydrogenation. V. V. Moshkovskii, N. I. Kabanov and P. N. Philippovich. *J. Phys. Chem.* (U.S.S.R.) 13, 320-40 (1959).—Data are given for the electrocatalytic hydrogenation of citric acid at electrodes with large (Cu, Ag, Ni, Pt, Au) and small (Ti, Fe) H<sub>2</sub> overvoltages, and in the presence of catalyst poisons such as K<sub>2</sub>AsO<sub>4</sub> and HgCl<sub>2</sub>. The "poisons" poison the first group of metals and activate the second up to a certain limit, e.g.,  $1 \times 10^{-4}$  mols./l. in alkali,  $6 \times 10^{-4}$  in acid for HgCl<sub>2</sub> on a Pt cathode and  $1 \times 10^{-3}$  mols./l. for K<sub>2</sub>AsO<sub>4</sub> on an Fe cathode, from which the Kubasov (cf. C. A. 53, 7564) "active ensemble" could be calculated: 2.1-2.4 for Pt, 2.0 for Fe. In this case the active centers have a lowered adsorption potential due to the effect of the "poison." On a clean Pt cathode the energy of activation between 0° and 51° is 0.96 ev., on a 1% alum 1.3 mol. thio: 0.22, and on an amalgamated Pt cathode 1.31 ev./mol. Comparison of the effects of poisoning of polarized surfaces of smooth and of platinumized platinum indicates that they are essentially the same. On Ag and Cu cathodes no reduction takes place with or without the presence of a "poison." Reptl. data are tabulated in 10 tables and 7 figs. The Edey-Orts-Volmer had the Rooden-Ridder conception of electrode processes are not applicable to electrocatalytic reduction. F. H. R.

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Catalysis, MTC,  
Chair of Gen. Phys.  
Colloidal Chem.  
Zur Med. Inst.

U-1613, 3 Jan 52

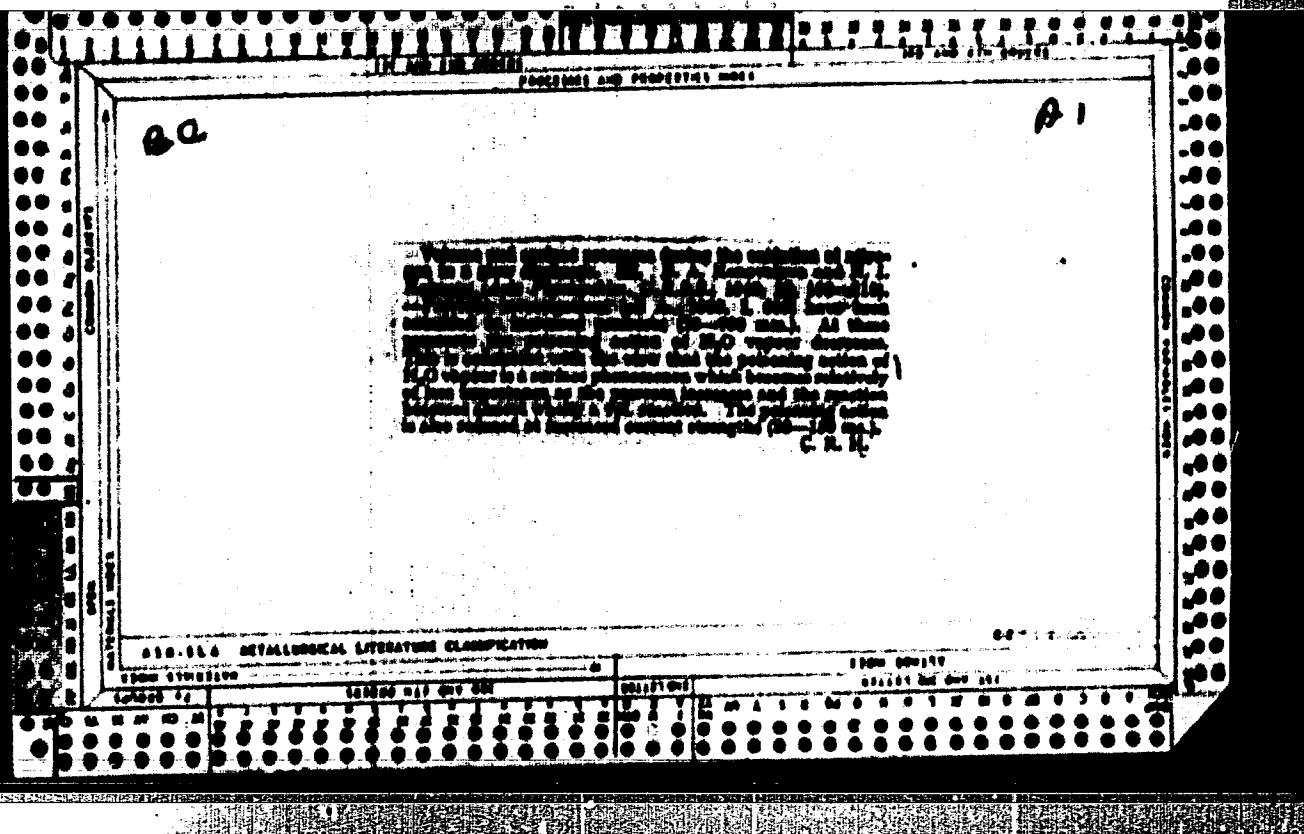
## A.I.O.L.A. METALLURGICAL LITERATURE CLASSIFICATION

SUBDIVISION		TOPIC AND SUB TOPIC		SUBTOPIC		SUBTOPIC		SUBTOPIC		SUBTOPIC		SUBTOPIC		SUBTOPIC		SUBTOPIC		SUBTOPIC		
COPPER	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20



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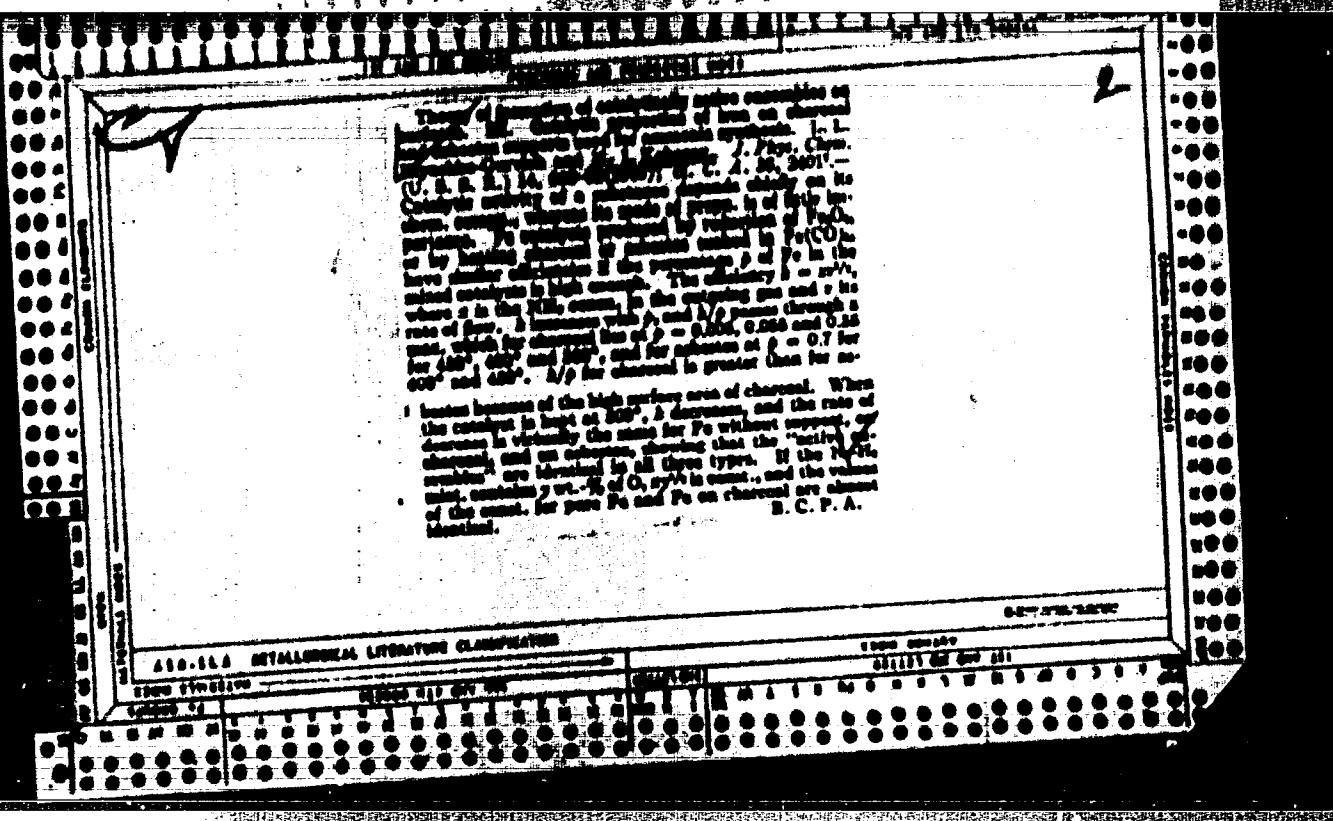
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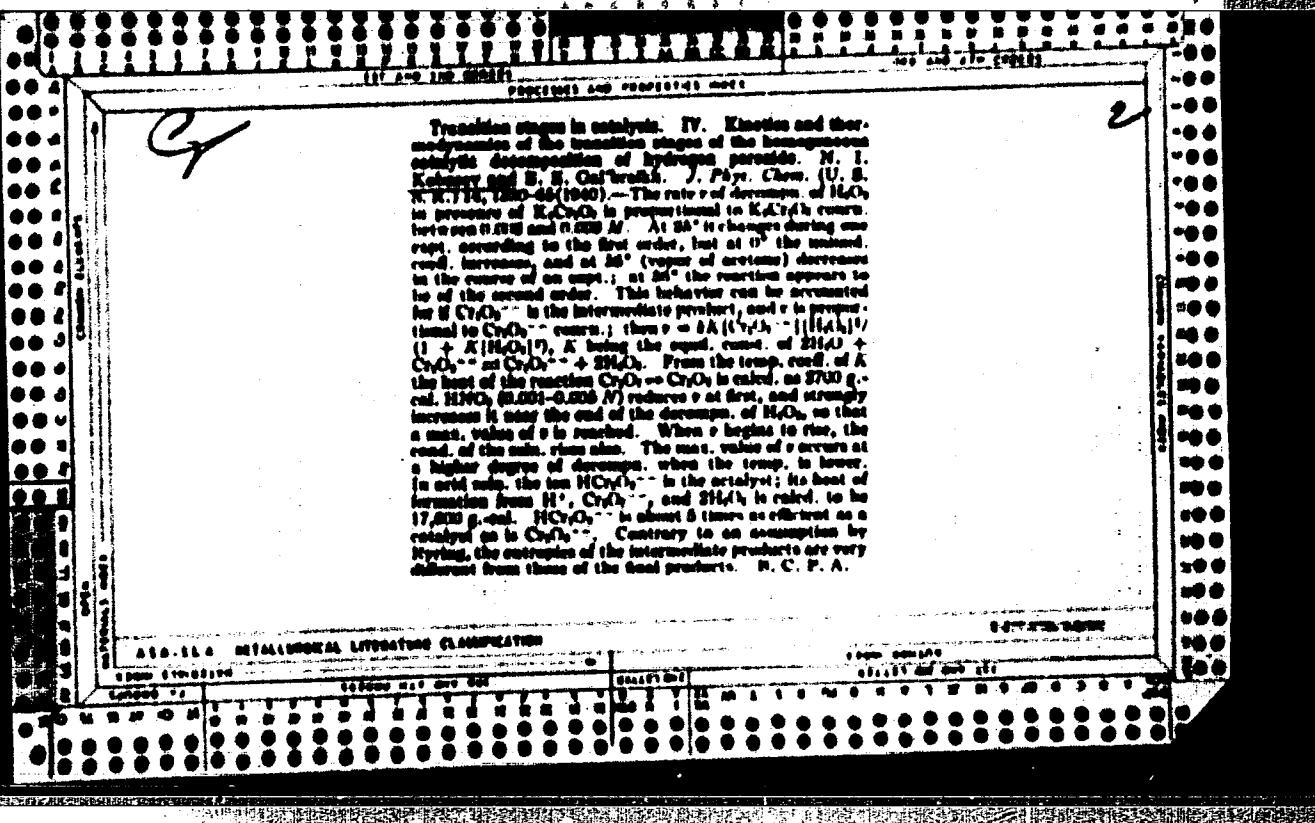
Theory of the formation of chemically active assemblies on surfaces. IV. Application of the theory to the polymerization of cyclohexene. M. I. Shemyakin, Akad. Nauk SSSR, 13, 1230 (1958) (U.S. German); cf. C. A., 52, 1964--March. Assuming that the motion of a molecular volume can act only on the activity of a single resonance molecule independently of processes occurring in neighboring molecules, i. e., a statistical rather than a thermodynamic distribution of polymer units, K. obtains the equation  $\dot{A} = A\sigma^{n-1}/\tau$  for the reduction of the initial concentration  $A$  by the act. of polymer  $\sigma$ , where  $n^2$  is the no. of resonance groups. The theory is able to explain many known, observed catalysis-polymer phenomena. Values are given for the NH<sub>3</sub> reaction on Fe, hydrogenation of the cyclohexene based on Pt, Pd, etc. The values of  $\sigma^2$  for a given polymerized catalyst are cited. For various reactions there are the same, and the values of  $\sigma^2$  for different catalysts run parallel with their melting points.  
P. H. Rathmann

A-1

BC

Volume and surface reactions in the oxidation of nitrogen by the oxygen molecule. N. N. R. A. Kostyleva and N. I. Tikhonova. Zhur. Fiz. Khim. 1968, 42(6), 1411 et seq. In the oxidation of  $N_2$  by  $O_2$  in a glow discharge is recorded by ESR method. It is assumed that the reaction is governed by  $v_1$ , the pressure of  $H_2O$  is that of the reaction is governed by  $v_2$ , the pressure of  $H_2O$  is that of the reaction is governed by  $v_3$ , and the difference  $v_4$  between the rate of closure of  $H_2O$  and  $v_1$  is the velocity of the surface reagent. The ratio  $v_1/v_2$  was 0.44% at 100 mm., 100 mm., and 215 mm. He was 0.44%, 0.44%, and 0.44% at 100 mm., 100 mm., and 215 mm. The ratio  $v_1/v_3$  showed a trend of 0.44% at 100 mm., 100 mm., and 215 mm. The ratio  $v_1/v_4$  increased with  $[H_2O]$  in air.  $v_1$  decreased with increasing  $[H_2O]$  pressure (100–215 mm.  $Hg$ ), and  $v_3$  is maximal at 100 mm., and falls at high pressures to zero or to negative values. The recorded value of  $v_4$  at high pressure is presumably due to a reduced extent of addition of adsorbed clusters to the walls. In air at 215 mm.  $v_4$  has maximal value for 0.44%–5.1% of  $H_2O$ , but (20%) in the discharge tube is lowered when  $[H_2O]$  rises. In air at 215 mm. both  $v_1$  and  $v_3$  increase when the current increases (20–100 mA) but the rise of  $v_1$  is 2 times as steep as that of  $v_3$ . The easy predominance of the  $N_2$  oxidation above that is of a non-thermal nature. J. J. H.

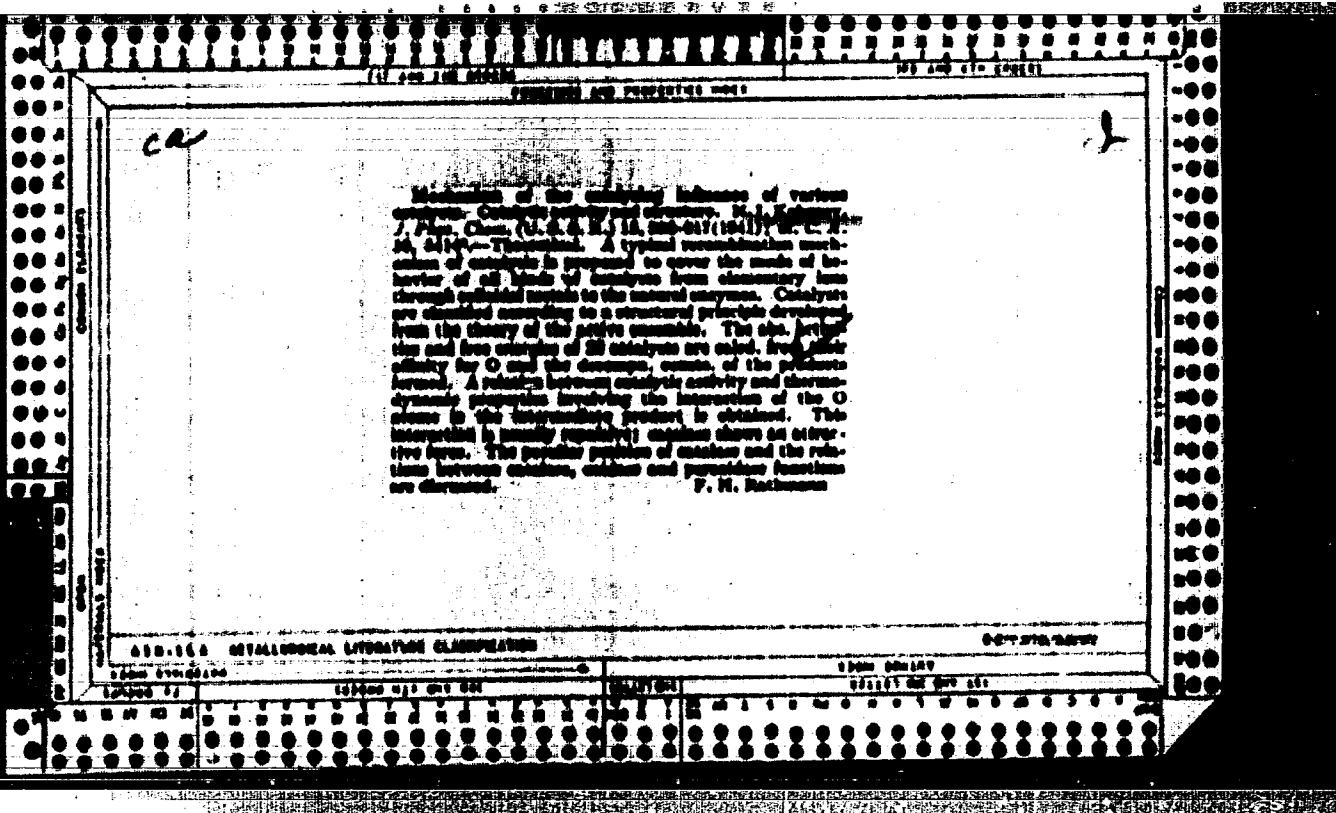


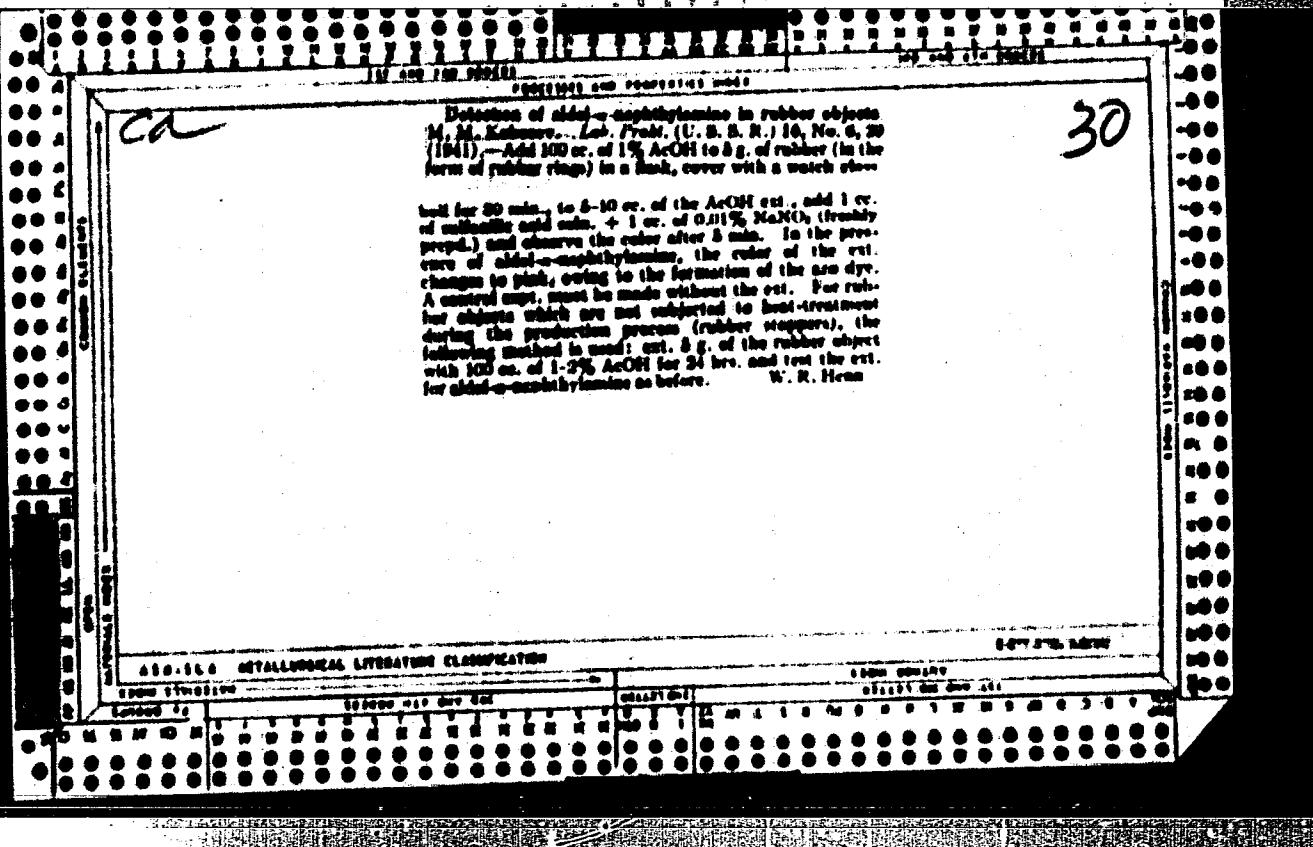


*Pg. 16.**11-5-1966, 100%*

Investigation of the effect of three impurities on the desorption process. A. L. Lippard, J. Phys. Chem. Anal., 1941, 14, 127-134, 273-280. The desorption temperature  $\text{pt}^\circ$  between 10° and 50° was 112° at  $\text{N}_2$ ,  $\text{CO}$ ,  $\text{C}_2\text{H}_2$ , and  $\text{CO}_2$  on  $\text{Ca}$ , and of 50-64° over  $\text{MgO}$ . The  $\text{pt}^\circ$  is not exactly with Langmuir's  $\text{N}_2$  on  $\text{Fe}$ , see previous. This can not completely with Lippard's equation and can be accounted for by assuming that an adsorbed film, lowers the adsorption potential  $U$  around it. The adsorption of  $\text{CO}$  on  $\text{Ca}$  occurring  $\text{U}/\text{U}_0 = 0.48-0.44$  c.c. per g. of  $\text{Ca}$  is not only < zero on pure  $\text{Ca}$  but the deviation of the desorption isotherms from Langmuir's equation is increased. If  $(\text{CN})_r$  were not hindering the desorption process this deviation would have been removed or reduced. The literature shows that adsorbed poison acts similarly toward the  $U$  of their adsorption nests. When the surface area of  $\text{Ca}$  is reduced by recrystallization at 200°, the amount adsorbed ( $\theta$ ) is less but the shape of the isotherm does not change.

B. The rate  $\sigma$  (i.e. per sec.) of desorption of  $\text{CO}$ ,  $\text{H}_2$ , propane, and  $(\text{CN})_r$  from  $\text{Ca}$ , and of  $\text{NH}_3$  from  $\text{Fe}$ , is measured at -40° to 150°. It rapidly decreases when  $\sigma$  diminishes, and the ratio  $\sigma/\sigma_0$  decreases at well, showing that  $U$  is the higher the smaller is  $\sigma$ . The increase of  $\sigma/\sigma_0$  with  $\sigma$  is less marked at higher temp.  $(\text{CN})_r$  reduces  $\sigma/\sigma_0$  and its increase with  $\sigma$  for desorption of  $\text{CO}$  from  $\text{Ca}$ ; this shows that the  $U$  of  $\text{CO}$  is lowered by the near-by nests. I. J. B.





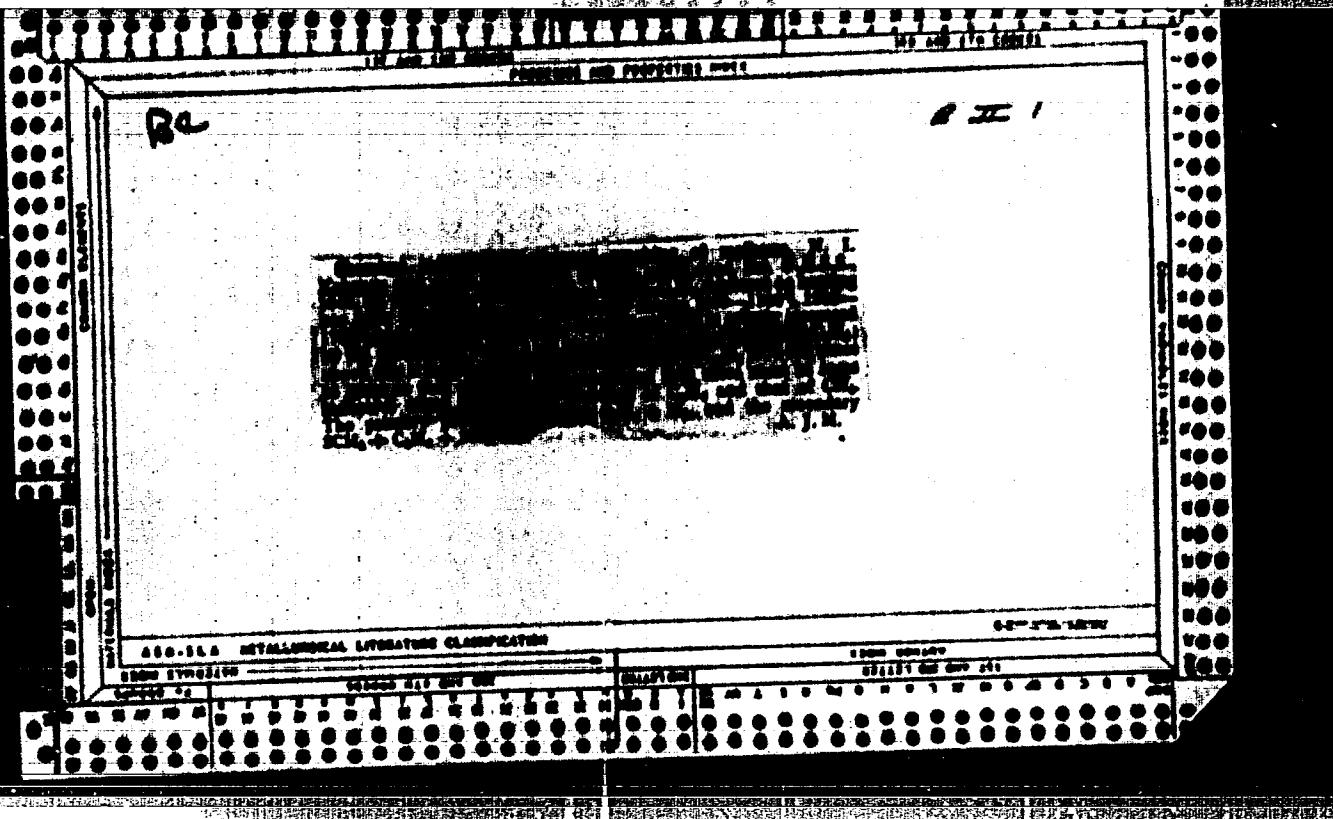
*Environ.*

Kinetics and energetics of the high-temperature cracking of  
methane to hydrocarbons. N. I. Kostanov and I. I. Kostanov (USSR).  
*Proc. Acad. Sci. U.R.S.S.*, 1941, Vol. 30, 38-53.—Equations are given  
for the kinetics of the various dehydrogenation reactions occurring  
in the cracking of  $\text{CH}_4$  to  $\text{C}_2\text{H}_4$  at high temp. The equilibrium  
constants are obtained. The high-temp. reactions, in contrast to  
those occurring at lower temp., do not take place at the walls.

A. I. M.

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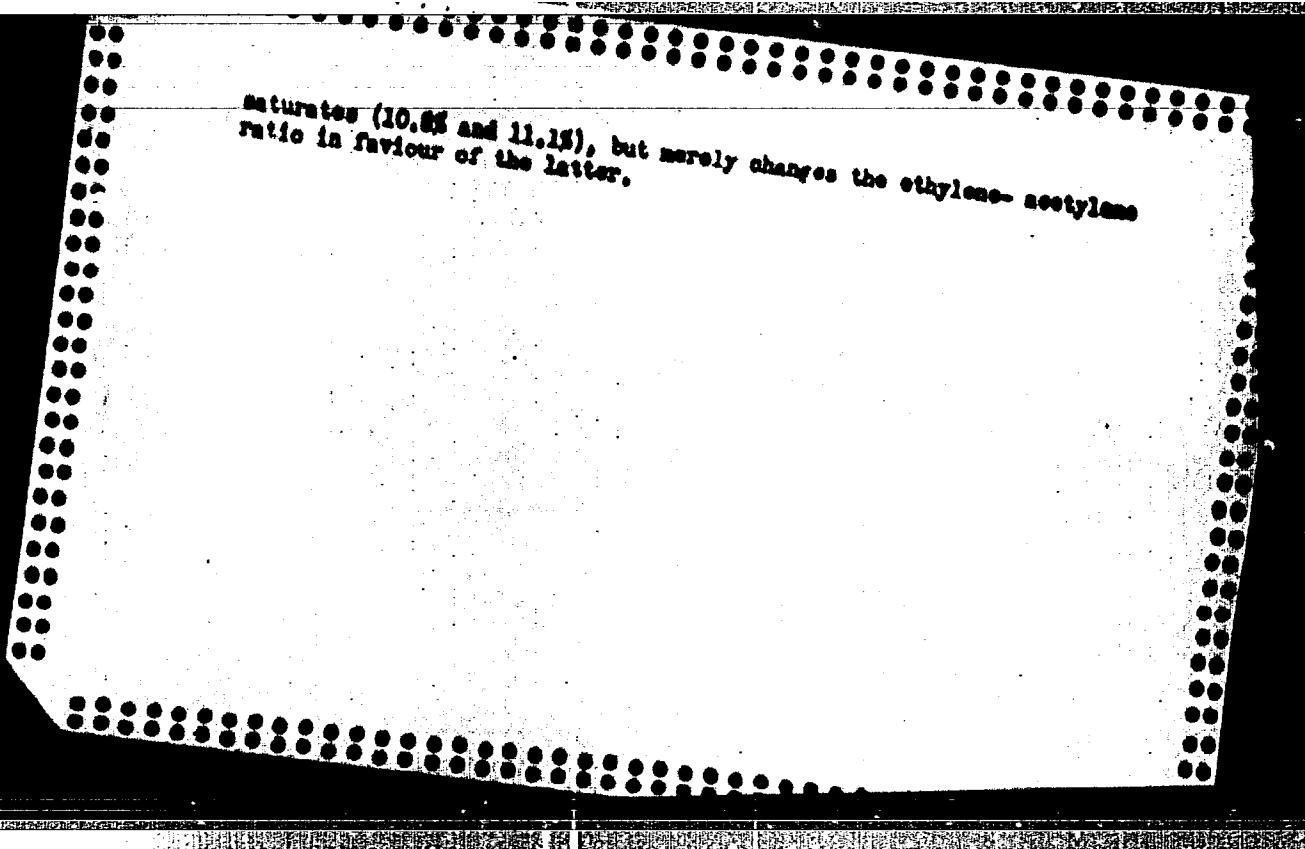
Activation characteristics of the thermal cracking of methane.  
N. I. Kabanov and N. N. Sosulin (Komp. rend. Acad. Sci. U.R.S.S.,  
1941, No. 223-226).—The kinetics of the cracking of CH<sub>4</sub> at low  
pressure, and when mixed with H<sub>2</sub>, have been investigated. In  
general, pressure accelerates the cracking process: 2CH<sub>4</sub> →  
C<sub>2</sub>H<sub>6</sub> + 2H<sub>2</sub> and C<sub>2</sub>H<sub>6</sub> → C<sub>2</sub>H<sub>4</sub> + H<sub>2</sub>. Dilution of CH<sub>4</sub> (butane) has  
approximately the same effect as a nine-fold decrease of pressure. The  
kinetic curves, obey the Arrhenius equation over a wide temp.  
range.

2463. IS QUENCHING NECESSARY IN THERMAL CRACKING OF METHANE TO ACETYLENE? Kobosov, M. I. (Compt. Rend. Acad. Sci. U.R.S.S., 1943, 52, (7), 261-264). K

Tests have been made on the influences of rapid and slow cooling of the reaction gases upon the yields of acetylene and ethylene in the cracking of methane-containing gases. The experiments were carried on in quartz, porcelain and carbon tubes in a platinum and in a Tammann stove at temperatures varying from 990 to 2000°C. The results of the experiments are given in a table. The data obtained show that when applied to the cracking of methane quenching is not only unnecessary, but, as a rule, even harmful. It is expedient to allow "after-cracking" after the gas has passed the heating zone. In this way one may increase the yield of unsaturates (and, thereby, cut down energy consumption) to 50%. In one test only cooling proved useful owing, probably, to a low rate of gas movement not consistent with the high temperature of the cracking process. Substitution of air cooling for special water cooling has no influence whatever upon the total yield of un-

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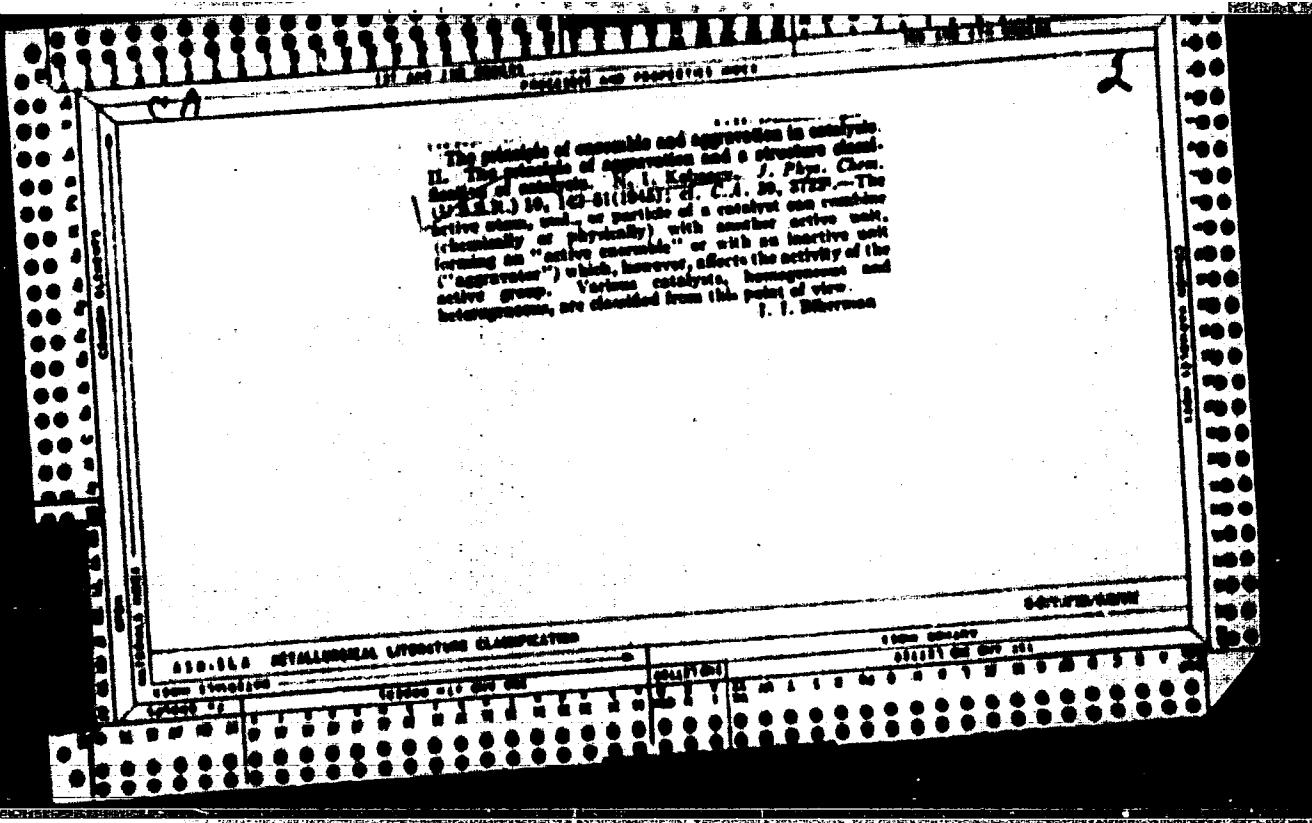
The kinetics of reduction and oxidation reactions can be measured by the method of cyclic voltammetry. In this method, the potential of the electrode is varied sinusoidally between two limits, and the current is measured at each instant. The rate of oxidation and reduction can be calculated from the derivative of the current with respect to time.

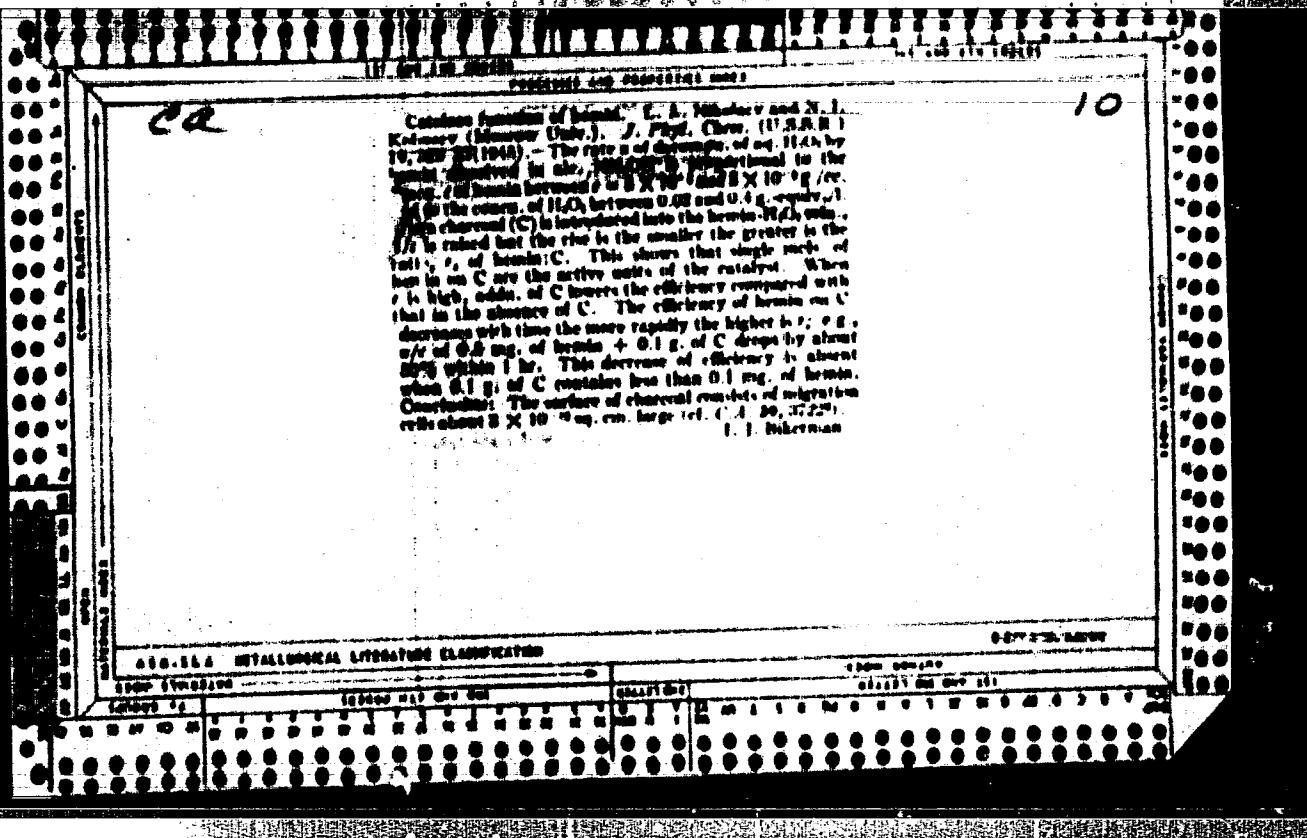
The rate of reduction of  $\text{MnO}_4^-$  in water is 0.25  $\text{A}/\text{cm}^2$  at  $25^\circ\text{C}$  on  $\text{SiO}_2$  gel; 0.1  $\text{A}/\text{cm}^2$  on charcoal, 0.1 for  $\text{Fe}^{2+}$  on charcoal, and 0.05 for  $\text{Cu}^{2+}$  on charcoal. The rate of reduction of  $\text{Cr}_2\text{O}_7^{2-}$  in water is 0.1  $\text{A}/\text{cm}^2$  on charcoal, 0.05 for  $\text{Fe}^{2+}$  on charcoal, and 0.03 for  $\text{Cu}^{2+}$  on charcoal. The rate of reduction of  $\text{NO}_3^-$  in water is 0.05  $\text{A}/\text{cm}^2$  on charcoal, 0.02 for  $\text{Fe}^{2+}$  on charcoal, and 0.01 for  $\text{Cu}^{2+}$  on charcoal. The rate of reduction of  $\text{Fe}^{3+}$  in water is 0.03  $\text{A}/\text{cm}^2$  on charcoal, 0.01 for  $\text{Fe}^{2+}$  on charcoal, and 0.005 for  $\text{Cu}^{2+}$  on charcoal. The rate of reduction of  $\text{Pb}^{2+}$  in water is 0.01  $\text{A}/\text{cm}^2$  on charcoal, 0.005 for  $\text{Fe}^{2+}$  on charcoal, and 0.002 for  $\text{Cu}^{2+}$  on charcoal. The rate of reduction of  $\text{As}^{3+}$  in water is 0.005  $\text{A}/\text{cm}^2$  on charcoal, 0.002 for  $\text{Fe}^{2+}$  on charcoal, and 0.001 for  $\text{Cu}^{2+}$  on charcoal. The rate of reduction of  $\text{Ag}^{+}$  in water is 0.002  $\text{A}/\text{cm}^2$  on charcoal, 0.001 for  $\text{Fe}^{2+}$  on charcoal, and 0.0005 for  $\text{Cu}^{2+}$  on charcoal.

The rate of reduction of  $\text{H}_2$  on  $\text{SiO}_2$  gel is 0.2  $\text{A}/\text{cm}^2$  for reduction of  $\text{MnO}_4^-$  in water, 0.1 for  $\text{Fe}^{2+}$ , 0.05 for  $\text{Cu}^{2+}$ , and 0.02 for  $\text{Mn}^{2+}$  on charcoal. The rate of reduction of  $\text{H}_2$  on  $\text{SiO}_2$  gel is 0.1  $\text{A}/\text{cm}^2$  for reduction of  $\text{Cr}_2\text{O}_7^{2-}$  in water, 0.05 for  $\text{Fe}^{2+}$  on charcoal, and 0.02 for  $\text{Cu}^{2+}$  on charcoal.

#### AIR-MAIL RETAINING INFORMATION CLASSIFICATION

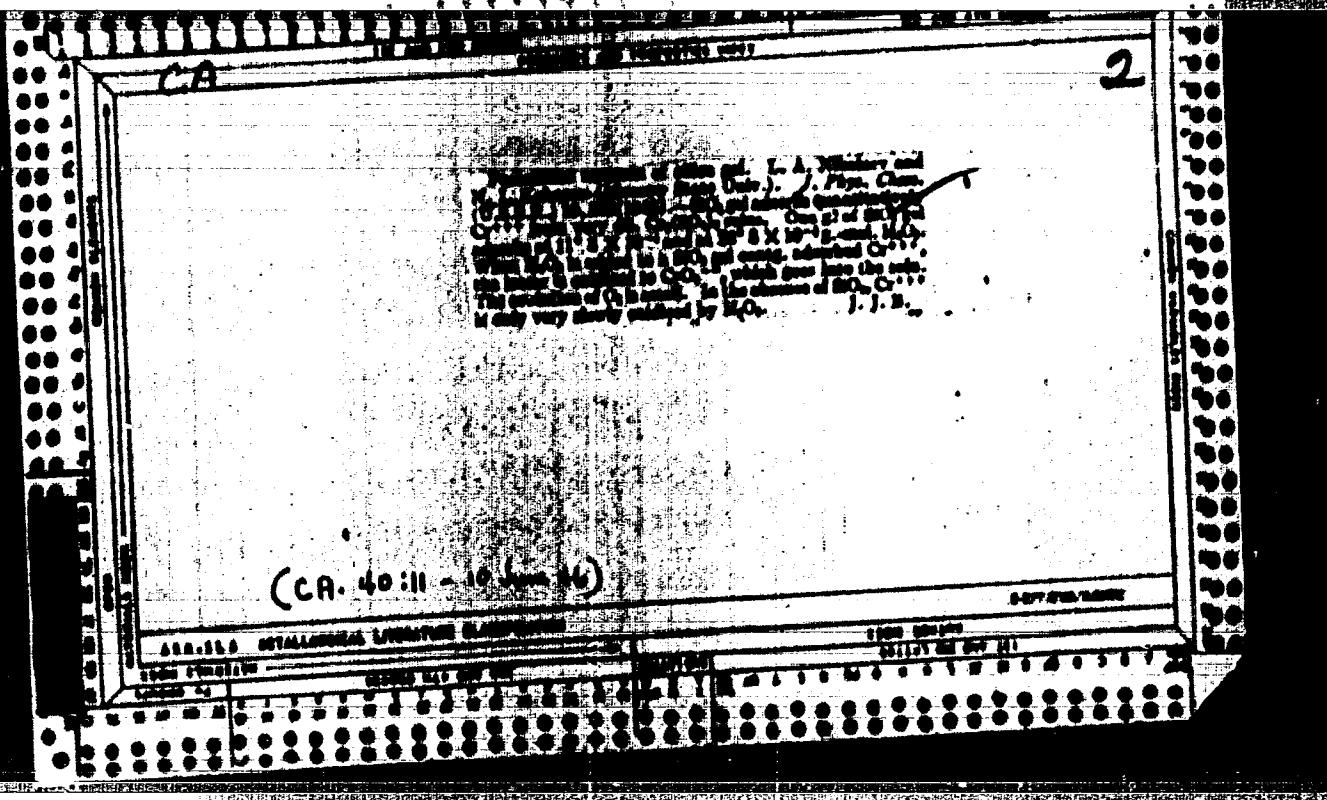
None





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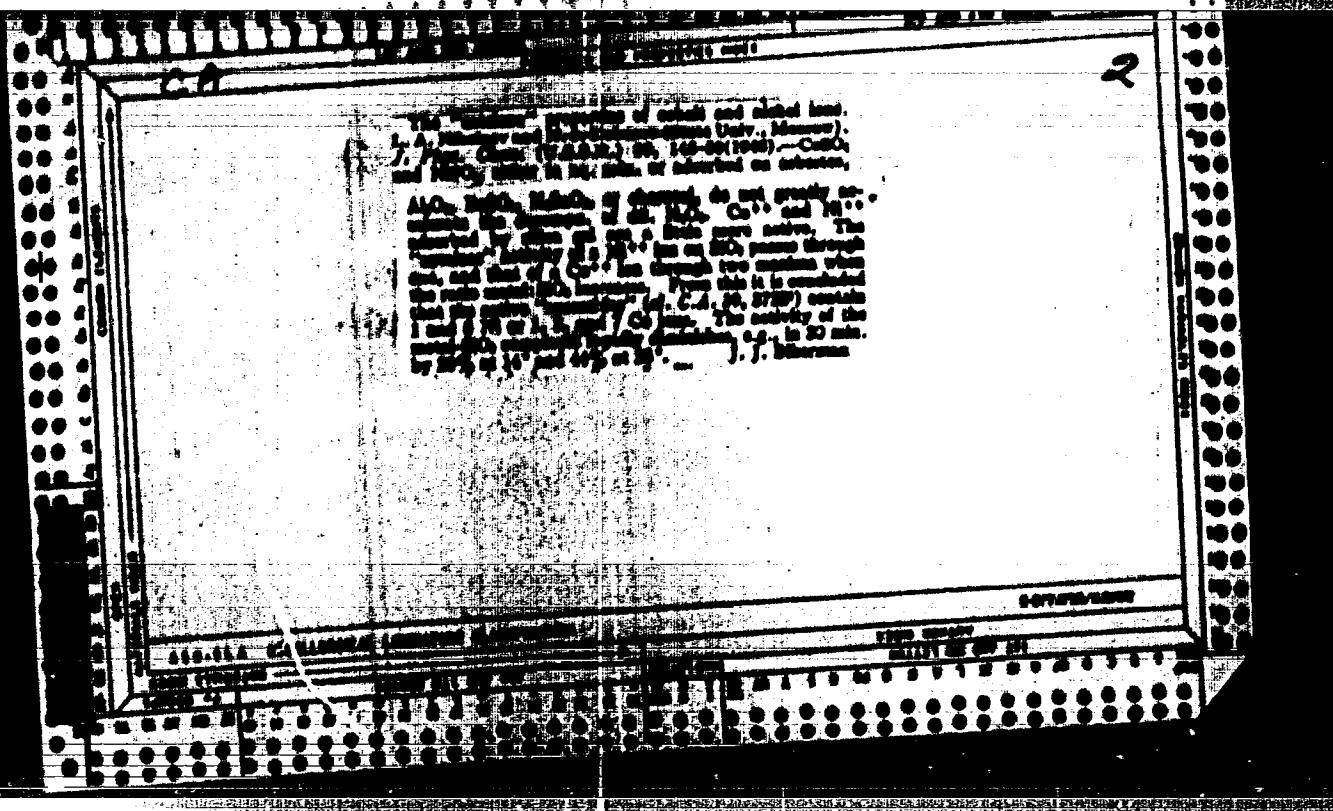
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KOBZEV, N. I.

Experimental studies of the intermediate stages of catalysis. IV. The kinetics and thermodynamics of intermediate stages in homogeneous catalytic decomposition of hydrogen peroxide. V. N. Kobzey and A. Galaktionov (Lomonosov State Univ., Moscow). *Acta Physicochim. U.R.S.S.*, 20, 470 (1946); cf. *C.A.*, 31, 3520; 27, 6720. Previous work on catalyst of  $H_2O_2$  decompr. by molybdate and chromate is summarized. New data are given for rate of decompr.  $V$  of  $H_2O_2$  in neutral solns. of 0.001-0.004 M dichromate at temps. from 0° to 60°.  $V$  is given by the expression  $\dot{V}(Cr_2O_7^{2-})K(H_2O_2)^2/(1 + K(H_2O_2)^2)$ , where chem. formulas in parentheses indicate total analytical molar amounts. This is precisely the formula expected for unlined, decompr. of a complex in equil. with 1 mol. of  $Cr_2O_7^{2-}$  and 2 mols. of  $H_2O_2$ , when  $H_2O_2$  is in excess.  $K$  is the equil. const. for formation and  $k$  the unlined, rate const. for decompr. of the complex  $Cr_2O_7^{2-} \cdot H_2O_2$ .  $K$  corresponds to  $\Delta F = -2700$  cal., independent of  $T$ , and  $\Delta S = 0$ ;  $k$  varies exponentially with  $1/T$ , and shows an activation energy of 15,780 cal. Similar analysis of previous data leads to a table of thermodynamic and kinetic constants for the possible complex ions:  $MoO_4^{2-}$ ,

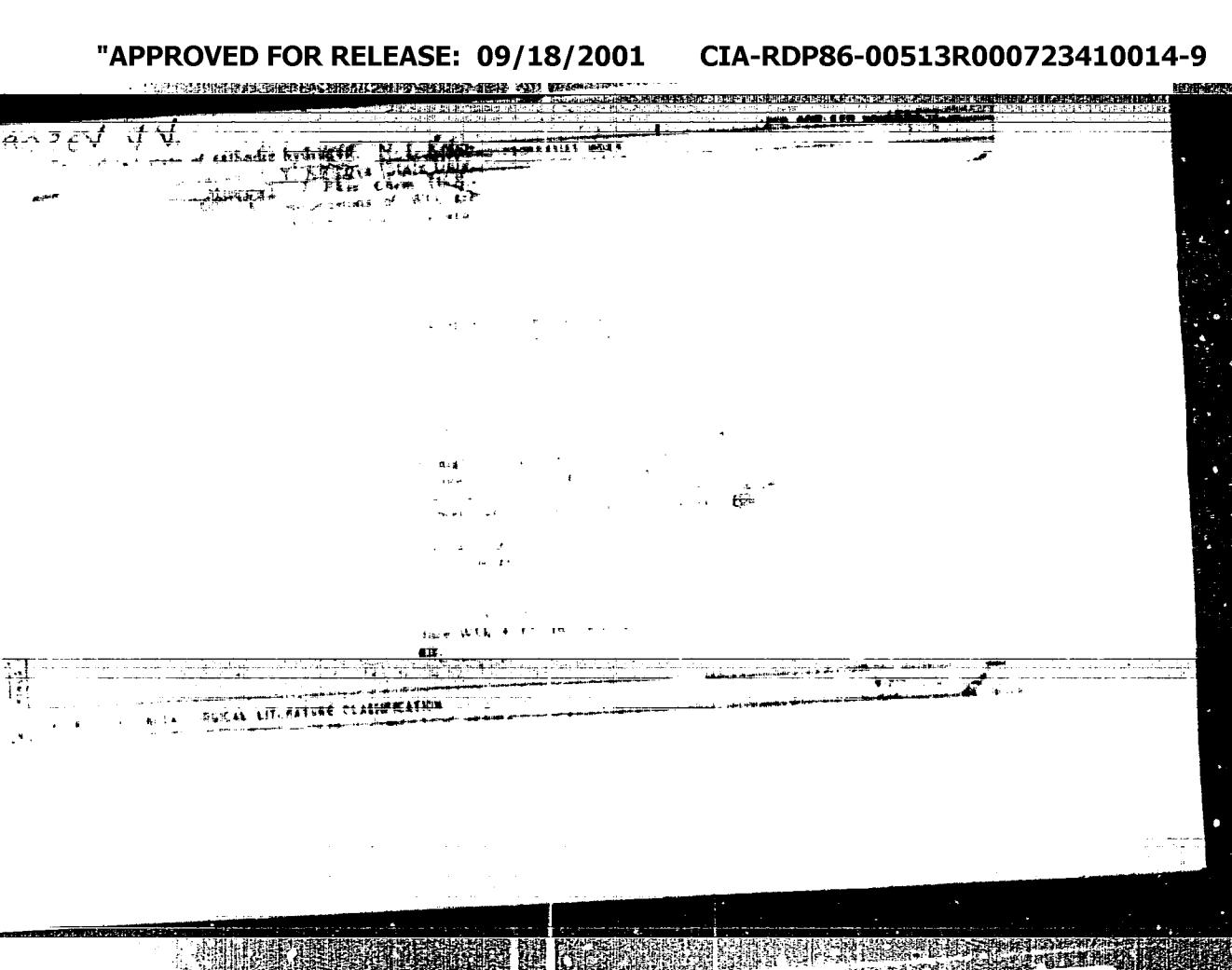
$WO_4^{2-}$ ,  $Cr_2O_7^{2-}$ , and  $HCr_2O_7^{2-}$ . The values for the different complexes are of the same order of magnitude except for  $HCr_2O_7^{2-}$ , which is thermodynamically more stable but decomps. faster as a result of an abnormally high frequency factor, which probably indicates a chain reaction. These intermediate compds. are very different from the "activated complexes" of Eyring since their entropies are not close to the entropy of the final reaction products.

A. D. Allen



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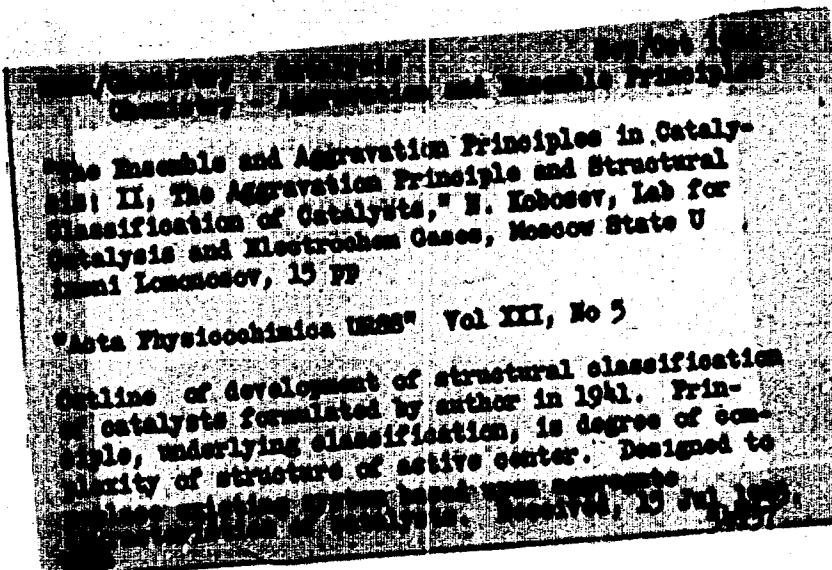
B.C.

"Resonable" and "aggravation" potentials in oxidation. I. Preparation method of catalysts having optimum in the range of potential between 1.5 and 2.0 V. V. L. Kabanov, V. V. Shchepetilnikov, I. V. Slobodchikova, N. V. Tikhonova, V. A. S. 1948, N. 1, 200-203; and I. G. Chukanova, N. V. Tikhonova, V. A. S. 1948, N. 1, 204-205. II. A. V. Kabanov. Preparation of a catalyst deposited in a dilute salt solution on an electrode covered by charcoal. Analysis of the composition of the active component of a number of cells separated by insulating membranes from the surface of a number of cells separated by insulating membranes of groups of 1, 2, . . . , n atoms within one boundary of the membrane of groups of 1, 2, . . . , n atoms within one cell in situ. If a membrane is sufficiently separated with a complex network of a number of pores, a layer of catalyst will cover all the surfaces of which this membrane is most branched. Analysis of experimental data of catalysts based on activity of the type anticipated. Metallic oxides catalysts appear to be active in groups of from 3 to 6 atoms. This type of activity is called "resonable" activity and is independent of the nature of the surfaces on which adsorption takes place. Resonable and the substantially active base of Ba, Ca, and the like is regarded as "aggravation" activity and it is considered that the inert surface or group to which the active base or metal is bound specifically "aggravates" its catalytic effect. O. D. S.

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Lab. for Catalysts  
+ Electrochemistry  
Gases, Moscow  
State U.

PA 54137

**KOBOSKI, N.**



relative action of various catalysts. The catalyst and structure, N. I. Kabanov (Moscow State Univ., Inst. Physicico-Chem. Probl., 21, 499-514 (1968) (in English).—The action of catalase and of other catalysts consists of speeding up the evolution of O<sub>2</sub> from H<sub>2</sub>O<sub>2</sub> is analyzed on the basis of 3 reactions (a)  $P + H_2O_2 \rightarrow P_O + H_2O$ ; (b)  $P + 2H_2O_2 \rightarrow P_O^2 + 2H_2O$ ; and (c)  $P_O^2 = P + O_2$ , where  $P$  is the catalyst. (a) and (b) are considered as rapid-equil. or steady-state systems having equil. constants  $K_1$  and  $K_2$ , resp. Reaction (c) is postulated as the slow step with a velocity const.  $k_3$ . Methods are shown for so plotting rate data as to yield values for  $K_1$ ,  $K_2$ , and  $k_3$ . The deduced true activation per active center at 0° is relative rates for the various catalysts were: Mo<sup>6+</sup>, CrO<sub>7</sub><sup>2-</sup>, WO<sub>4</sub><sup>2-</sup>, and I, 0.1; P<sub>2</sub>O<sub>5</sub><sup>11+</sup>, 1.0; Cr<sub>2</sub>O<sub>7</sub><sup>2-</sup>, 11.0; Fe<sup>3+</sup> on charcoal, 100; humic, 30 to 60; humic

on charcoal, 100; catalyst,  $5 \times 10^3$ ; PbO<sub>2</sub> and MnO<sub>2</sub>, 10<sup>3</sup>; and Pt-black and, 10<sup>2</sup>. The const.  $A_0$  in the equation  $A_0 = h\omega e^{-\epsilon/\theta}$ , where  $\epsilon$  is the energy of activation of reaction (c), is equal to  $\sim 10^{20}$  throughout the series; this shows that the enhanced activity of the more complex catalyst must be attributed primarily to a lowering of the activation energy.  $K_1$  is calculated from  $K_2$  and  $k_3$ ,  $\Delta F_1$  for reaction (a) and  $\Delta F_2$  for reaction (b). A plot of  $\log A_0$  against  $\Delta F_1 - \Delta F_2$  gives data for all catalysts to fall on 3 straight lines, one for the supported catalysts including catalase, humic on charcoal, and PbO<sub>2</sub> on charcoal, and the other for the homogeneous catalysts including humic, P<sub>2</sub>O<sub>5</sub><sup>11+</sup>, and MnO<sub>2</sub> *in situ*. The increasing activity for each series corresponds to decreasing repulsion between the O atoms in  $P_O^2$ ; for catalase,  $\Delta F_1 - \Delta F_2$  is neg., corresponding to attraction rather than repulsion between the O atoms. A picture of the intermediate complex holding the 2 O atoms is deduced in which thermodynamic repulsion between the O atoms decreases as the total amt. of supporting material to which the active centers are attached increases. The interrelation of catalase, peroxidase, and oxidase functions is also discussed. P. H. B.

AB-15A METALLURGICAL LABORATORY CLASSIFICATION

04-17-2007

TYPE SYMBOL

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CA

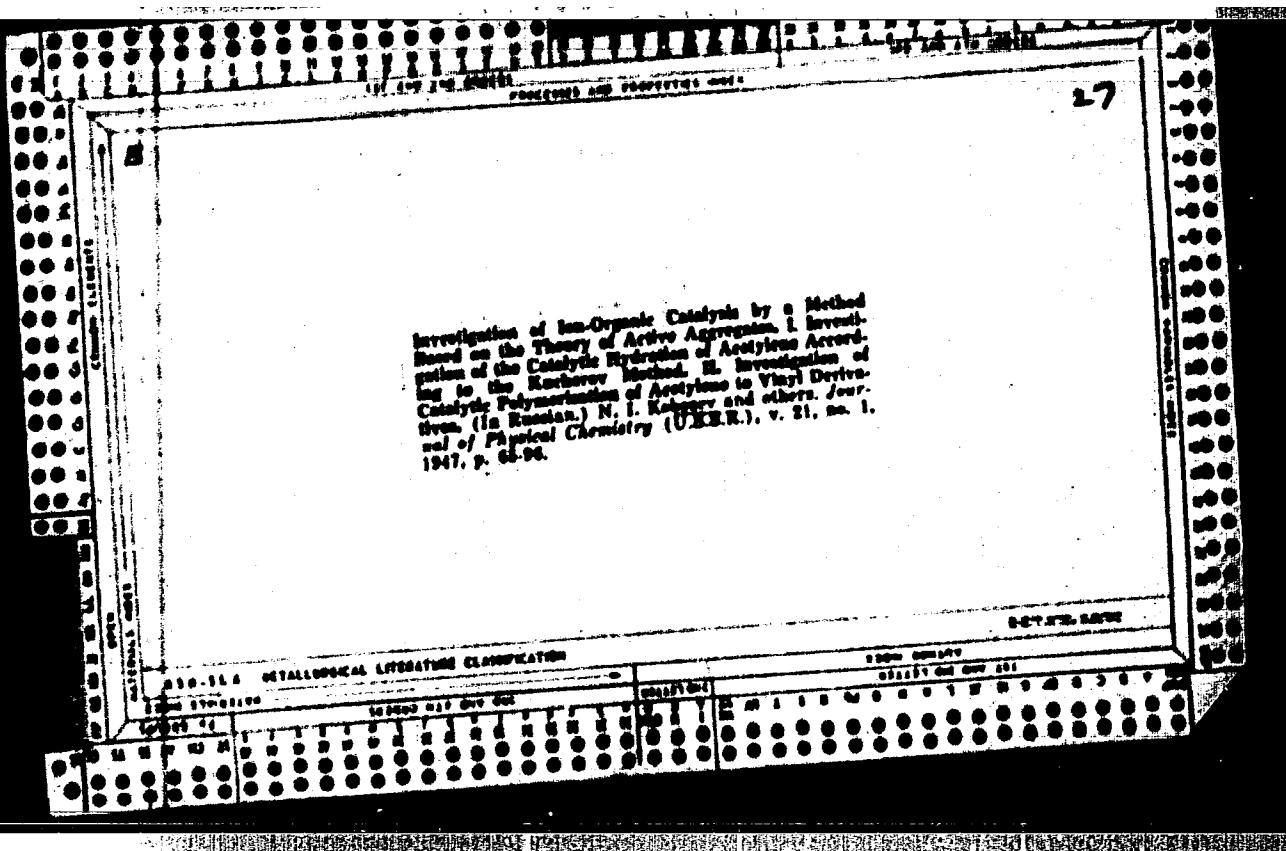
Specific effects of minor amounts of heavy metals on the rate of adsorption-desorption. N. I. Klyushnev and I. A. Zelenovich (Leningrad State Univ., Leningrad). *Comp. rend. acad. sci. U.R.S.S.* 53, 131-4 (1946); *C.A.* 36, 8729. - Various catalysts were prepared by simultaneous or successive adsorption on magnetite charcoal (surface area approx. 300 sq. cm./g.) from mixtures of the salts. In each case the amount of the first metal was held at 0.1% of the total catalyst, and that of the 2nd metal was varied:  $\text{Fe}^{+++}$ ,  $\text{Cu}^{++}$ ,  $\text{Ca}^{++}$ ,  $\text{Pb}^{+++}$ ,  $\text{Ag}^+$ . The activity of the resulting catalyst was measured by determining the no. of g. mol. of sucrose transformed per min. The activity of one metal was strongly affected by the addition of other metals of another, and this effect was almost the same for cations (dissociation of  $\text{H}_2\text{O}_2$ ) or anions (oxidation of  $\text{Na}_2\text{SO}_3$ ) except that catalysis was inhibited whereas oxidation was enhanced. For example, the addition of 0.005%  $\text{Cu}^{++}$  to 0.1%  $\text{Fe}^{+++}$  increased the oxidation activity 7 times and decreased the reduction 15 times. As added amounts of a metallic element were added to the catalyst, the change in activity, however, has, approaching a certain limit, which was rapidly reached, and was only slightly more than the original increment. The phenomena were no doubt related to the stage of adsorption of the ions. In a homogeneous medium the phenomena may be reversed. The addition of  $\text{Cu}$  to  $\text{Fe}$  not only inhibits oxidation, but actually weakens oxidation. These phenomena are considered part of the general subject "effect of traces" and as such may be of importance to the explanation of the functions of boron, silicon, aluminum, and the like. Peter M. Bernays

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Pedagogical Inst.,  
Yaroslavl.

## ABE-11A METALLURGICAL LITERATURE CLASSIFICATION

CLASSIFICATION		SUBDIVISION		COLLECTOR		CROSS REFERENCE											
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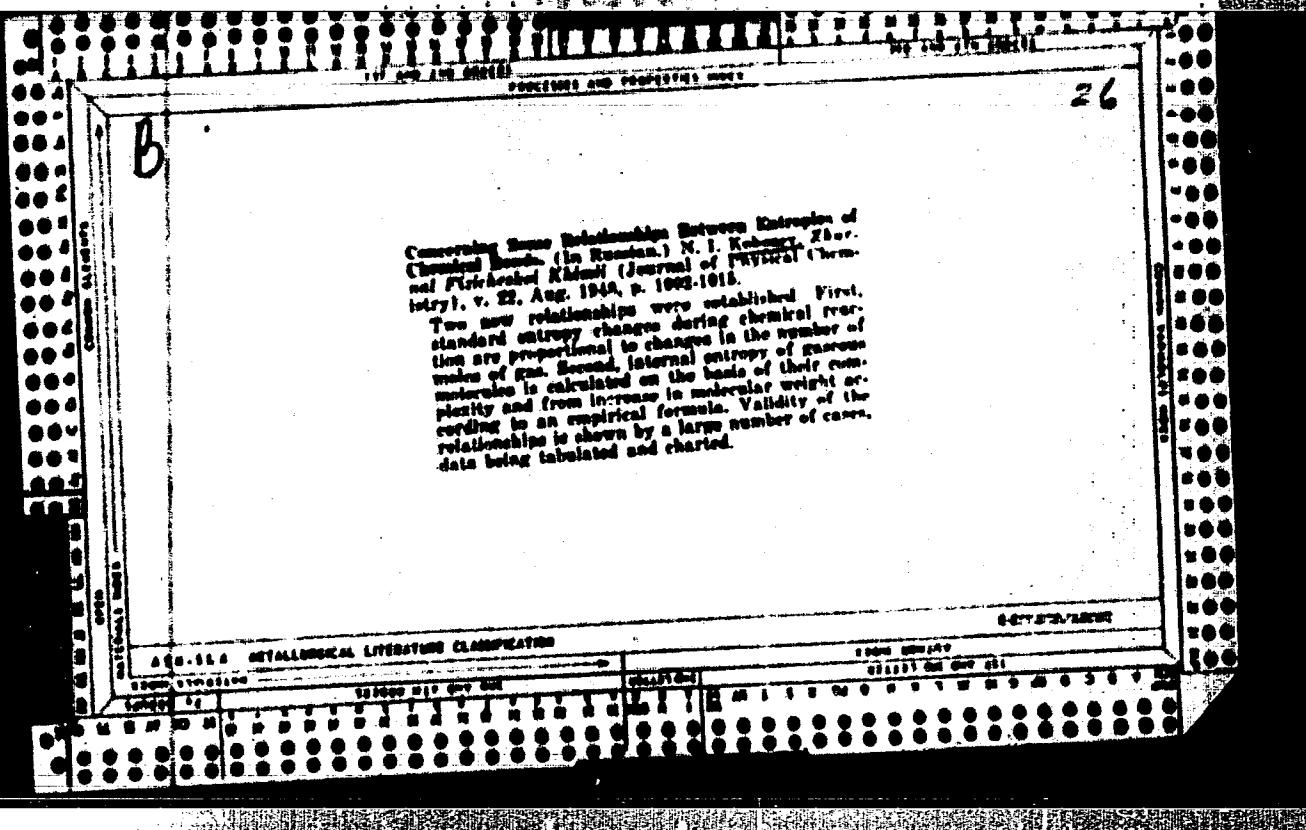
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The behavior of catalase in an adsorption layer. [A. A. Mikhaylov and N. I. Kabanova, *Voprosy Radiofiziki i Radiokhimii*, No. 1, p. 111 (1947) (in Russian).]—When graphite powder was used as an adsorbent it was found that, owing to carbon, the specific activity dropped with an increased surface carbon. This indicates that only a single mol. of catalase was active in the adsorption layer. A small amt. of humic did not change the activity of catalase, but a small amt. of catalase destroyed the activity of humic completely.  
Friedel A. Neiger.

## ADM-51A METALLURGICAL LITERATURE CLASSIFICATION



KOBZOV, N. I.

N. I. Kobzov and V. V. Nenbanova, A letter to the Editor. p. 1511.

Refers to previous publications by the writers (J. Phys. Chem. (USSR) 20, 653 (1946) and Z. Elektrochem. 54, 592 (1930) and letter concerning it by Bagotzki and others (Dokl. Akad. Sci. (USSR) 53, 5 (1944) and J. Phys. Chem. (USSR) 21, 241 (1947)).

Lab. of Catalysis and Gas Electrochemistry  
Moscow Lomonosov State University  
Chair of Chemistry of the Second Moscow Medical Inst.  
June 12, 1948

JO: Journal of Physical Chemistry (USSR) 22, No. 12 (1949)

111111, No 1.

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111111/111111 - Biology

Jan 1948

"Elements of the General Theory of Vector-Brownian Processes, and the Laws of Biological Kinematics,"  
N. I. Kobozev, 50 pp

"Byullet Moek Obshch Izgvt Pri, Otdel Biolo" Vol LIII,  
No 1

Describes experiments conducted to solve two problems:  
1) relationship between vector and Brownian components  
in trajectories; and 2) make trajectories "Brownian"  
by taking vector potential inherent in organisms, in  
this case insects. Editors note that this work, in  
parts, closely follows material published by E.  
Schrödinger in his book "Life From the Standpoint of  
Physics."

61366

c 1

Active compounds of platinum in oxidation reduction and  
hydrogenation processes. N. I. Kostomy and N. A.  
Kostomyan. Zhur. Fiz. Khim. 23, 302-305 (1949);  
U.S.P. 2,578,721. A chloroplatinate was deposited on  
active C or Al<sub>2</sub>O<sub>3</sub> and used as catalyst. From the varia-  
tion of the catalytic activity A with the degree of reduc-  
tion n the no. % of Pt atoms in the active "monohydride" and  
also in the no. % of Pt atoms in the active "dihydride" were calcd. In de-  
composition of H<sub>2</sub>O<sub>2</sub> n was 1 and 4-6 (on C and Al<sub>2</sub>O<sub>3</sub>), in oxida-  
tion of H<sub>2</sub> 1 (on C and Al<sub>2</sub>O<sub>3</sub>) and 6 (on Al<sub>2</sub>O<sub>3</sub>), in hydro-  
genation of maleic acid and PhCOCl 2 and 6 (on C), and in  
reduction of  $\beta$ -nitrophenoxide (I) and phenyl acid (II) 1 and 6  
(on C). When the catalysts were prepared by depositing  
[PtCl<sub>6</sub>]<sub>n</sub> on C, the curve  
[PtCl<sub>6</sub>]<sub>n</sub>[CH<sub>3</sub>CH<sub>2</sub>Cl<sub>2</sub>] / H<sub>2</sub>D on C, the curve  
"A/n against n" decreased monotonically, where n is  
calcd. from the formula n = 1 in hydrogenation of maleic  
acid, PhCOCl, I, and II. Because the starting substance  
contains 2 atoms of Pt in the molecule, the true n = 2, and the  
decreasement in the intensity of I and II is attributed to  
deactivation due to formation of monohydride and dimeric Pt.  
J. J. Ullman

*Inc Catalysts & Gas Electrolyzer*

410-162 METAL DEPOSITION LABORATORY CLASSIFICATION

RECEIVED BY [unclear] 12-17-57  
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KOZEEV, N. I.

"Structure of Disperse Catalyst and Carriers in the Light of the Theory of Active Combinations," Zhur. Fiz. Khim., 23, No. 12, 1949. Moscow OL St U im M. V. Lomonosov, Lab Catalysis and Gas Electrochem, Moscow. -c1949-.

KOBOZEV, N. I.

"Synthesis and decomposition of ammonia in electrical discharges II.  
Sensitized synthesis of ammonia in a glow discharge," Yu. V. Filippov, V. P.  
Lebedev, V. V. Zel'man and N. I. Kobozev (Lomonosov State Univ., Moscow). Zhur.  
Fiz. Khim., 24, 1009-15 (1950)  
For abstract of article see card for Yu. V. Filippov.

CA

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The problem of the micro doses in chemistry and in biology (growth substances as activators of catalytic systems). I. A. Zubovskiy and N. I. Karpova. (Moscow Univ.), Russ. Chemica 14, 19-28 (1971); cit. 7, p. 63, RICB. -- The ion-sorption catalyst consisted of 1%  $V^{+++}$ ,  $Cu^{++}$ , and  $Ag^{+}$ , deposited on sugar C. The catalytic activity (H<sub>2</sub>) was first measured. After the deposition of various doses of org. acids or phytohormones, the activity of the catalyst was again determined. A comparison of these 2 activities showed the accelerating or inhibiting effect of micro doses of org. substances on the activity of absorption catalysts. Small doses of growth substances (0.0005-0.005%) activated the catalysts, whereas larger doses (0.01-0.1%) inactivated them. As is known, the same type of action is shown by the phytohormones in stimulating and in inhibiting plant growth. The av. activating effect by phytohormones on the Cu, Ag, and V catalysts was 20, 22, and 11%, resp. Fatty and aromatic acids were inactive. Aliphatic hydroxy acids (glycolic, lactic) sharply inactivated the catalysts. Fatty acid activated the Ag catalyst, but was without effect on the V catalyst. The activation of absorption catalysts by phytohormones could be very accurately measured, and the results were always reproducible, thus providing a physico-chemical method of characterization of phytohormones. H. Priestley.

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RECORDED, NO. 1.

N. I. Kobozev. Some remarks concerning the article by D. V. Sokol'skii and K. I. Stender,  
"The role of the carrier in heterogeneous catalysis." p. 375

M. V. Lomonosov Moscow State Univ. Lab. of Catalysis & Gas Electrochem., Oct. 17, 1950

SO: Journal of Physical Chemistry, Vol. 25, No. 3 (March 1951)

CA  
Theoretical errors in the works of A. N. Proskin, Z. A. Isha, and V. S. Berezin [on theory of hydrogen overvolt-  
age]. *Zhur. Fiz. Khim.* 23, 1111-16  
(1949).—The theory of H<sub>2</sub> overvoltage of K. and Nebranov  
(C.A. 30, 1930) is defended. Attempts are made to show  
that the arguments raised against it by Proskin's school  
(Berezin, et al., C.A. 41, 2701A, 6475d) are theoretically  
incorrect because they purport to disprove a reaction mech-  
anism (stationary state) by thermodynamic calcs. (equil-  
state).  
Michel Boujart

KOBOZEV, N. I.

Overvoltage

Adsorption theory of hydrogen overvoltage. I. Overvoltage and energy of M-H bond.  
Zhur.fiz.khim. 26 no.1. '52.

Monthly List of Russian Accessions, Library of Congress, September 1952. UNCLASSIFIED.

KOBOZEV, N. I.

USSR/Chemistry - Catalysts Jan 52

"Problem of the Paramagnetic State of Catalytically Active Iron Layers (Errors in S. L. Kiperman and M. I. Temkina's Article 'Investigation of the Magnetic properties of Iron-Carbon Catalysts')," V. B. Evdokimov, I. N. Ozeretskovskiy, N. I. Kobozev, Moscow State University M. V. Lomonosov

"Zhur Fis Khim" Vol XXVI, No 1, pp 135-144

Sufficiently dil layers of Fe on carbon are completely paramagnetic, i.e., the Fe is atomic rather than cryst. Catalytic activity of ammonia Fe catalysts, etc., is due to atomic "ensembles" rather than Fe or any other element in the cryst state. There is a sharply lowered ferromagnetism in comparison with ordinary iron even in highly concd Fe layers on carbon. Diln of the Fe adsorption layer on carbon leads to a strong increase of paramagnetism due to Fe atoms. The same phenomenon was observed with adsorbed  $\text{Ni}(\text{NO}_3)_2$ . Increase of magnetic susceptibility and ferromagnetism in the samples after oxidation were observed.

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